

Assessment of Oxy-Combustion Impacts on Boiler Design and Performance During 15 MW_{th} Pilot-scale Testing

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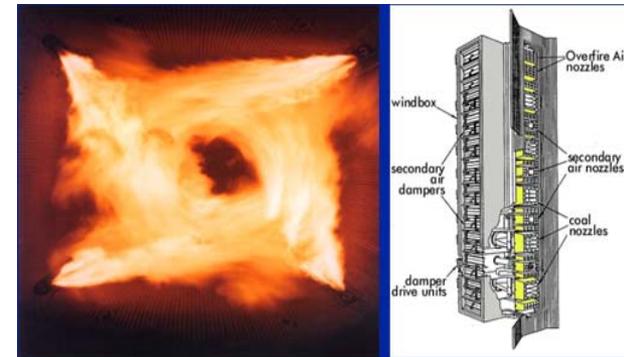
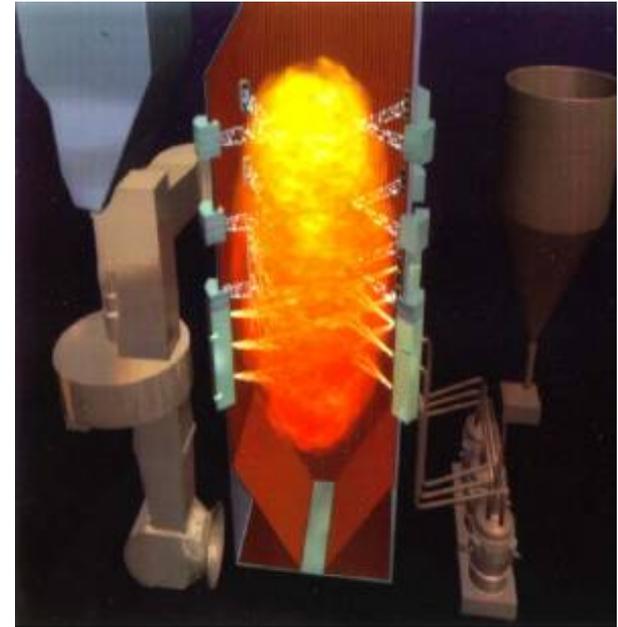
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Project Objectives

Develop oxyfuel T-fired boiler system for high CO₂ content gas. Specifically,

- Design and develop an innovative oxyfuel firing system for T- fired boilers
- Evaluate the performance in pilot scale tests at 15 MW_{th} BSF – including **combustion, heat transfer, pollutant emissions**, and deposition and corrosion
- Evaluate and improve engineering and CFD tools for oxy-combustion by applying detailed test data obtained



Project Team:

- Alstom –Boiler Laboratories
- Alstom – New & Retrofit Boiler Business
- DOE NETL  
- ICCI – Illinois Clean Coal Institute 
- NDIC – North Dakota Industrial Commission 
- Utility Advisory Group



Ten Utility Members:

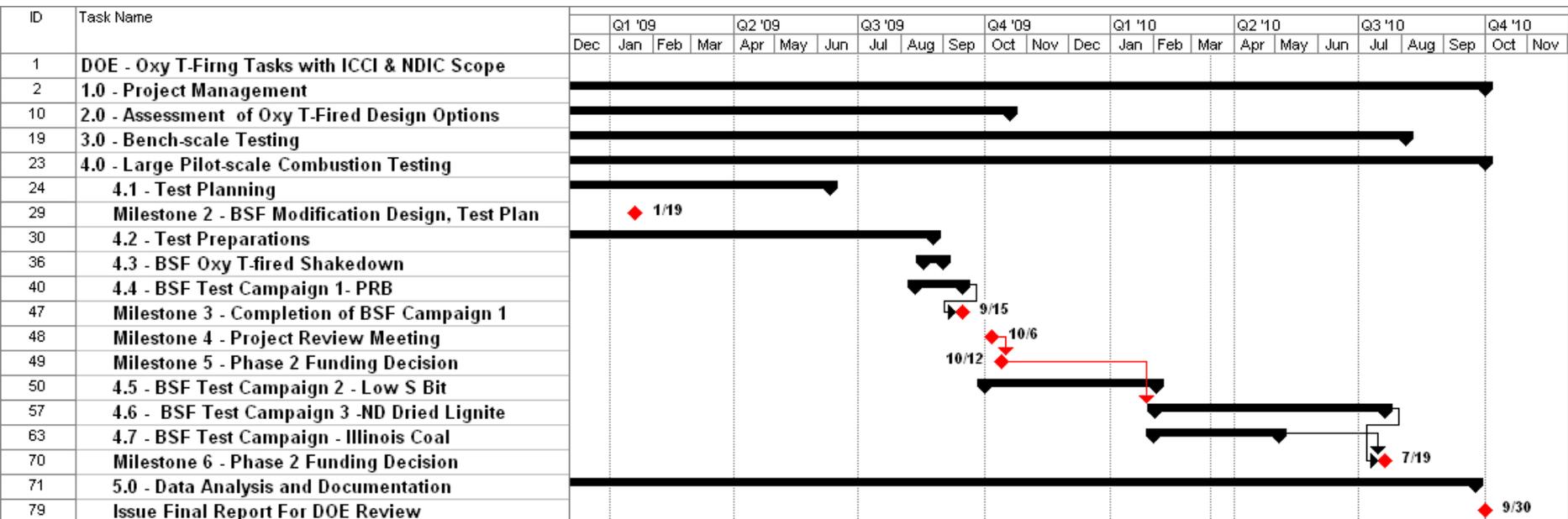
Ameren
ATCO
Dominion Energy
Great River Energy
Luminant (TXU)
LCRA and Austin Ene
MidWest Generation
NB Power
OG&E
Vattenfall



Schedule



- Project Budget: \$8.8M
- Project Duration: 24 Months
- Start: October 2008
- First Test Campaign: September 2009
- Complete Project: September 2010



Scope Accomplished

- Process and CFD Screen Completed
- BSF Modifications For Oxy-Firing Completed
- BSF Commissioning Completed
- BSF Campaign 1 Testing Completed – Subbituminous
- BSF Campaign 2 Completed – Low Sulfur Bituminous
- BSF Campaign 3 Completed – High S Illinois Bituminous

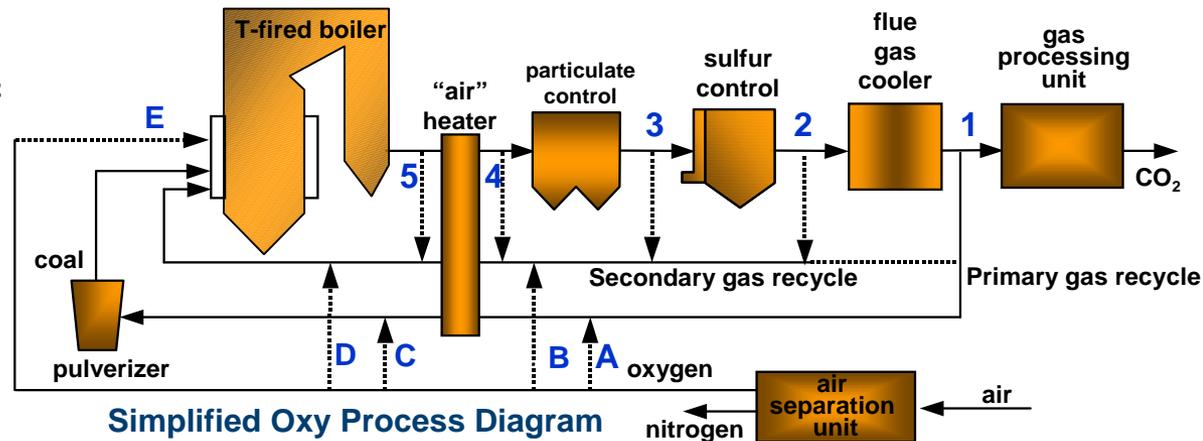
Plan

- ND Lignite Testing
- Complete Data Analysis and Tool Validation

Process Options: Techno-Economic Evaluation

Major Variables:

- Gas Recycle Take-off Locations
- Oxygen Injection Locations
- Oxygen Heating
- Recycle Rate / Furnace Surfacing

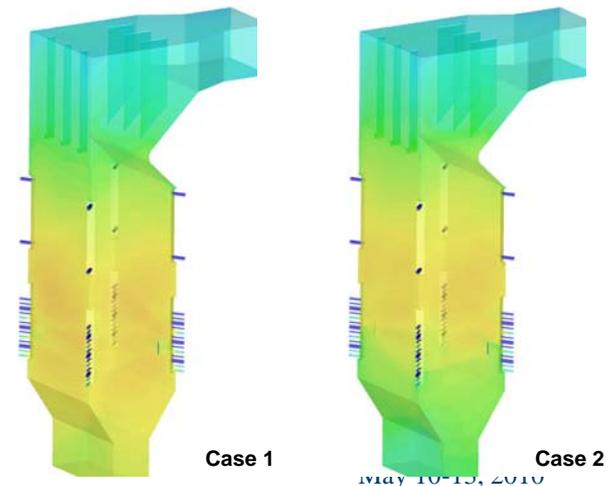


15 MWt BSF Oxy Simulations

CFD Modeling: Detailed Predictions

Additional Variables:

- Oxygen Injection Method, Conc., Distribution
- Windbox Design (Compartments, Vel., Angle)
- OFA Design (Location, Vel, Angle)



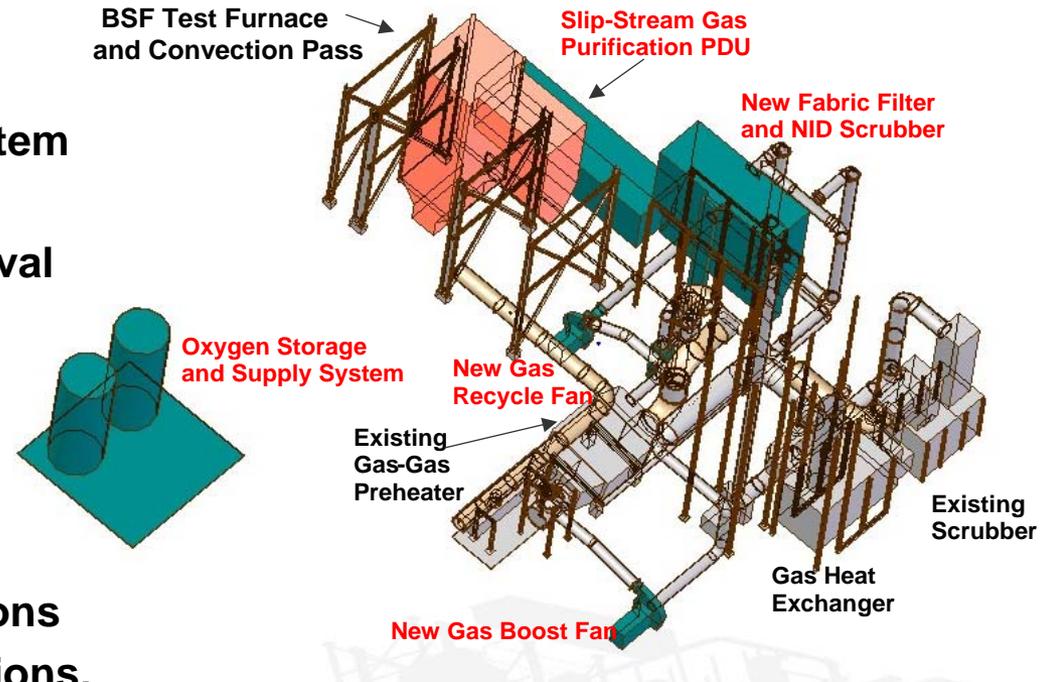
Major New Equipment

- Oxygen Supply and Injection System
- Gas Recirculation Systems
- Fabric Filter for Particulate Removal and NID SO₂ Scrubber
- Instrumentation and Controls

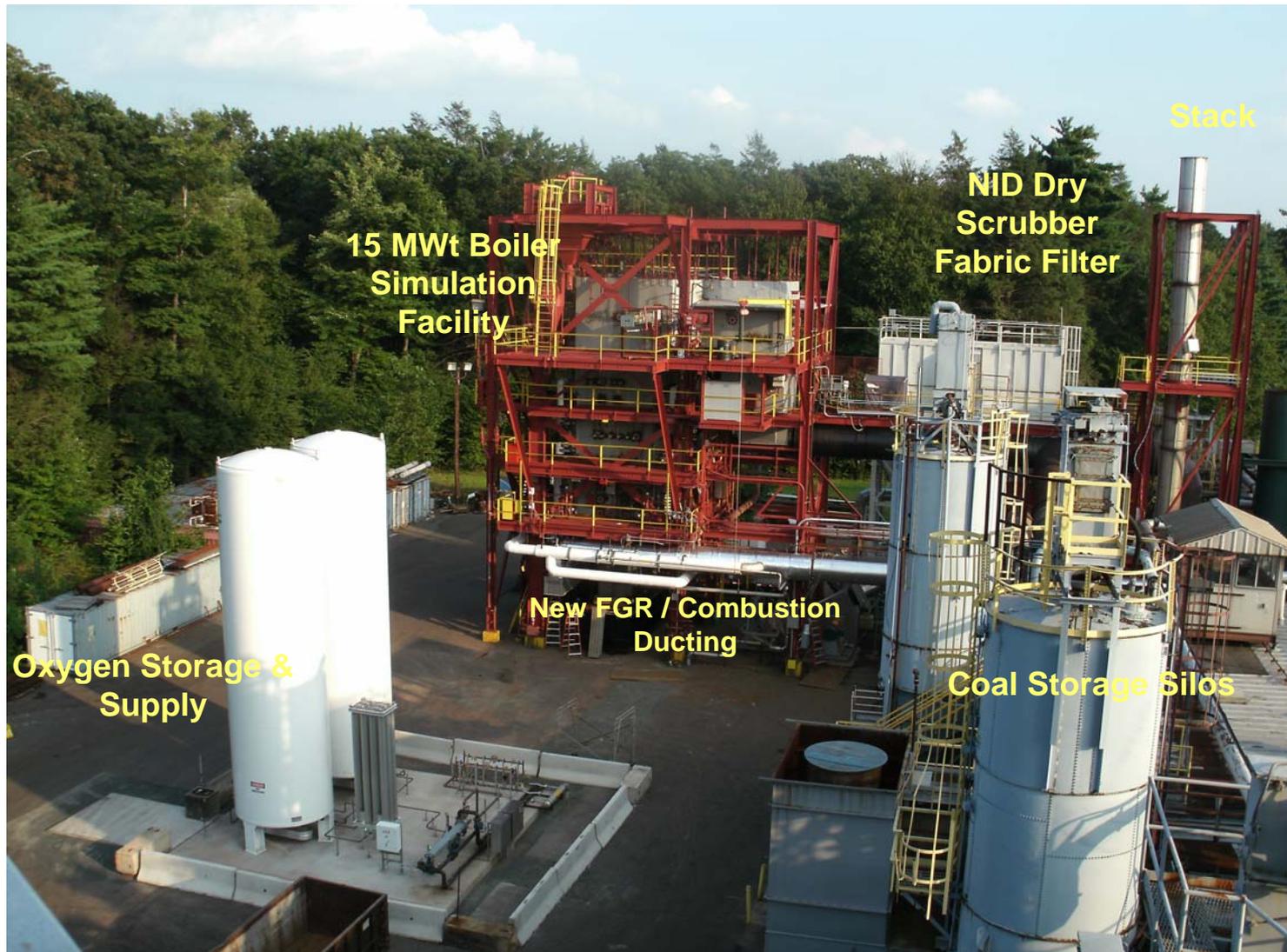
Design for Operating Flexibility

- Operate Both Air- and Oxy-fired
- 5 Different Operating Configurations
- Control of Oxygen Injection locations, concentrations, etc.

Integration of Slip-Stream Gas Purification Unit



15 MW_{th} BSF After Oxy Modifications



Primary Test Variables

- **Gas Recycle Take-Off Location**
- **Gas Recycle Flow Rates**
- **Oxygen Injection**
- **Total Excess Oxygen / O₂ Conc. at Economizer Outlet**
- **Windbox & OFA Design – Arrangement, Velocity**
- **Operating Load/ Turndown**

Data Acquisition System (More than 1,000 I/O Points)

- Continuous Logging of Operating Conditions (System Flow Rates, Gas Compositions, Temperatures, Pressures, Valve Positions, etc.)
- Continuous Heat Transfer Measurements (4 Waterwall Test Panels, 6 Continuous Test Loops Across Furnace Vertical Outlet Plane, 3 Deposition/Corrosion Probes)

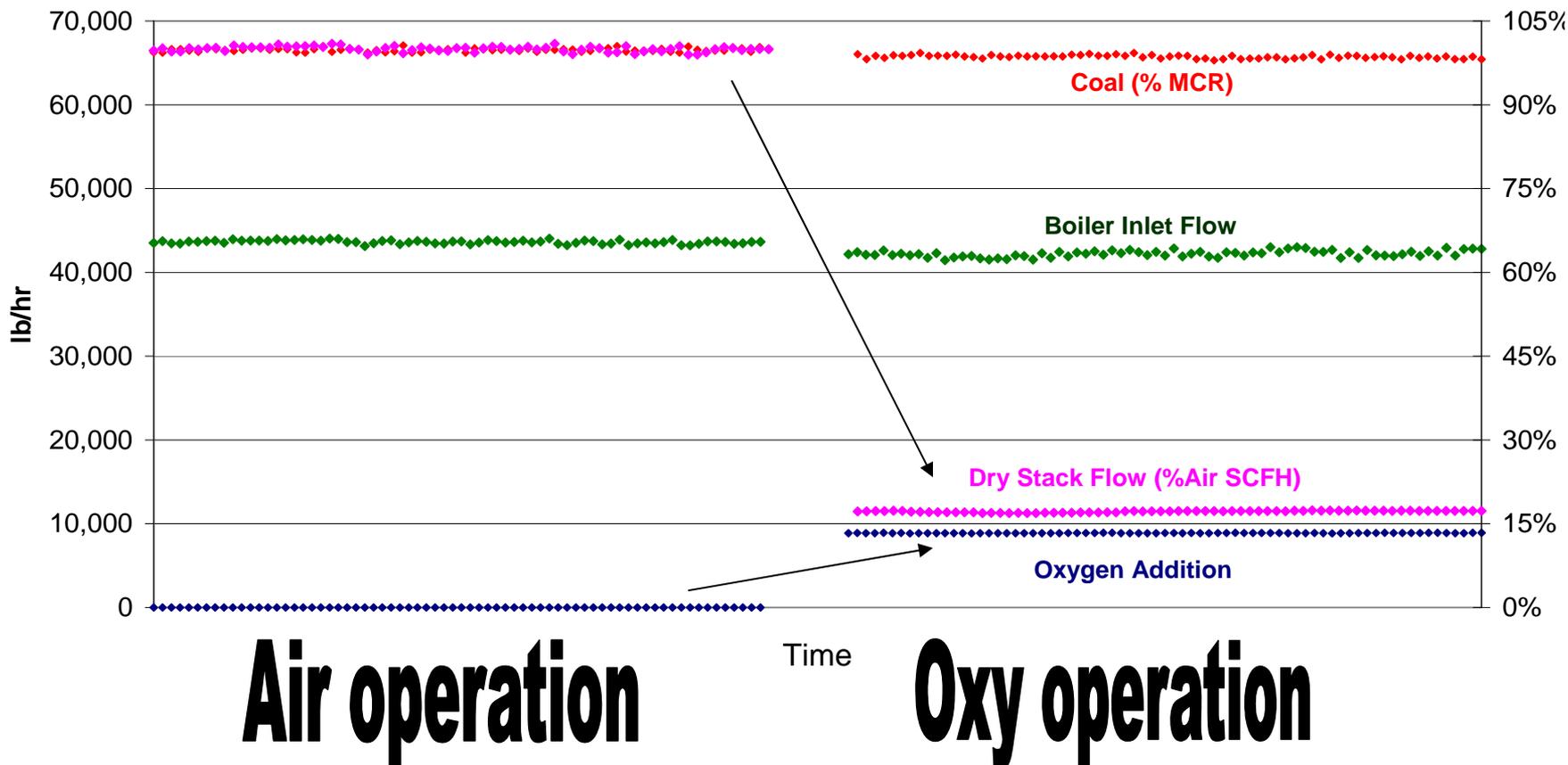
Probe Measurements

- Furnace Gas Temperatures and Gas Species Mapping
- In-Furnace Heat Transfer (Total Heat Flux Probes, Ellipsoidal Radiometer Probes)
- Mercury Measurements
- SO₃ Measurements
- Particulate Trace Metals

BSF Campaign 2 - Low S Bituminous Steady State Mass Flows



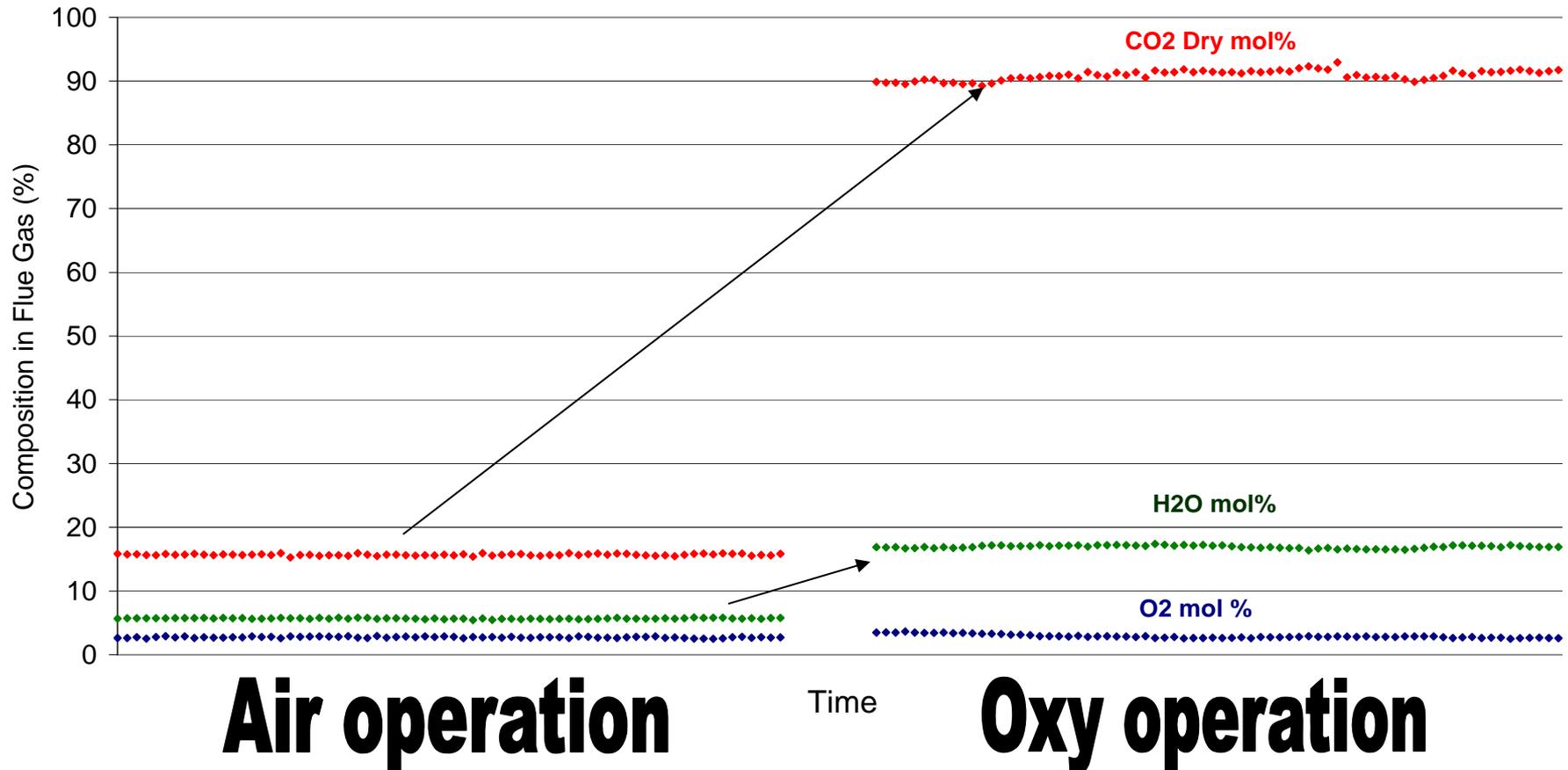
- Dry Stack flow is roughly 20% of Air Fired Volume.



BSF Campaign 2 - Low S Bituminous Steady State Gas Species Compositions

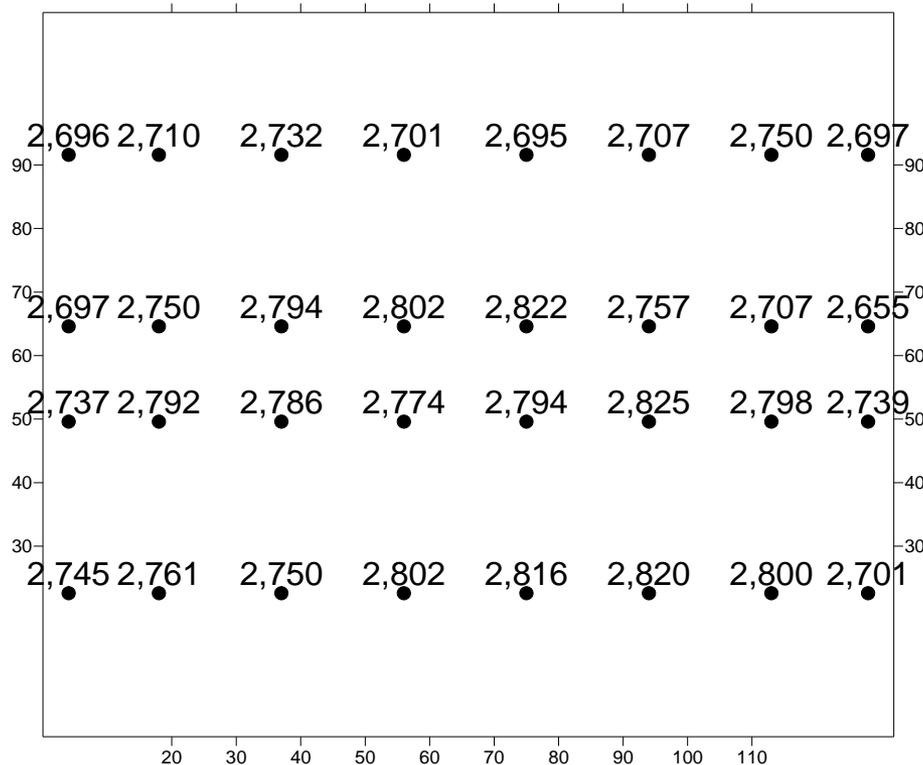


- Able to maintain 90% CO₂ (dry) in flue gas
- Conditions varied from 1.5 to 2.5% Air In Leakage to the facility



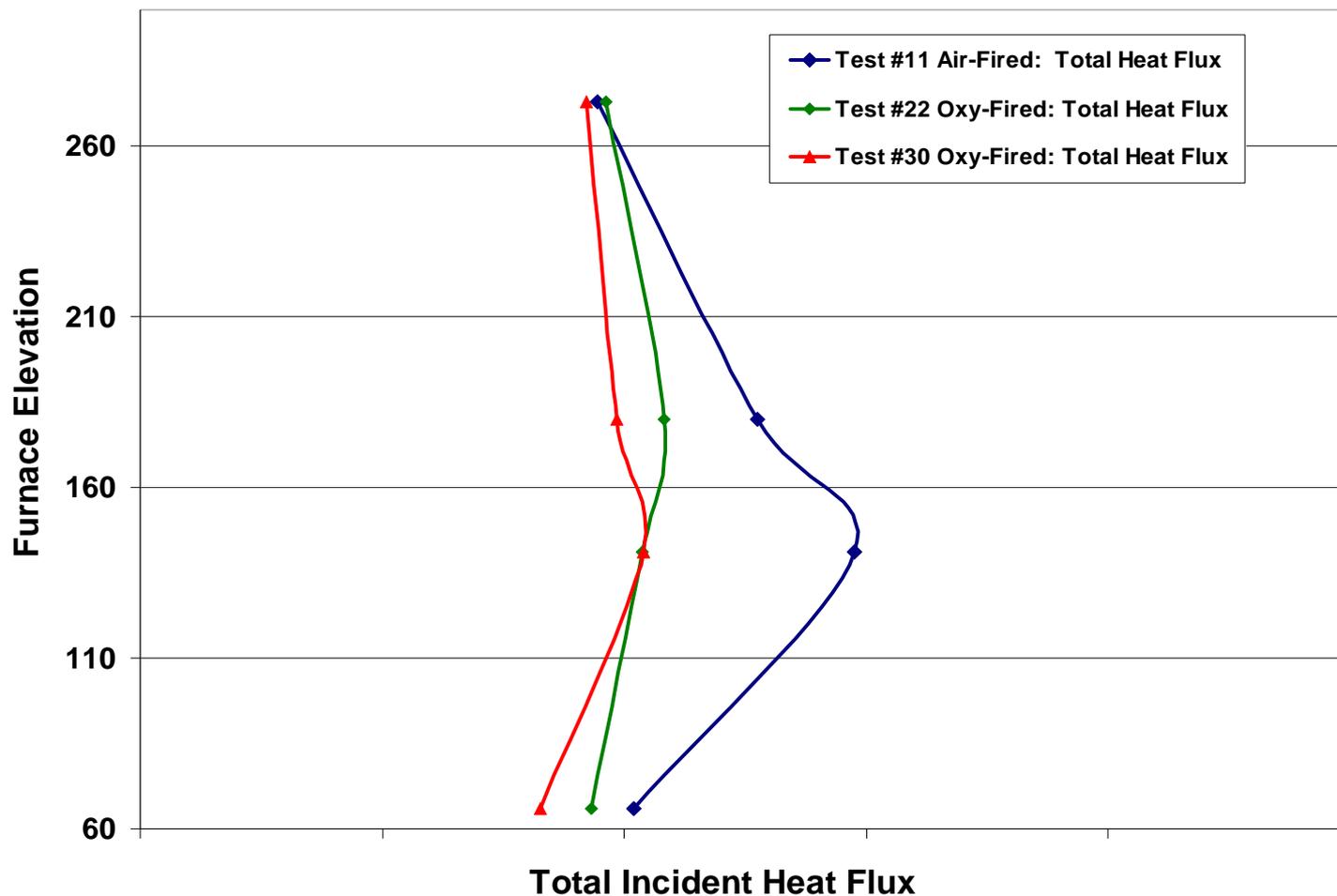
Sample Planar Temperature Profile Between OFAs

Temperature
Plane 180
Test #54



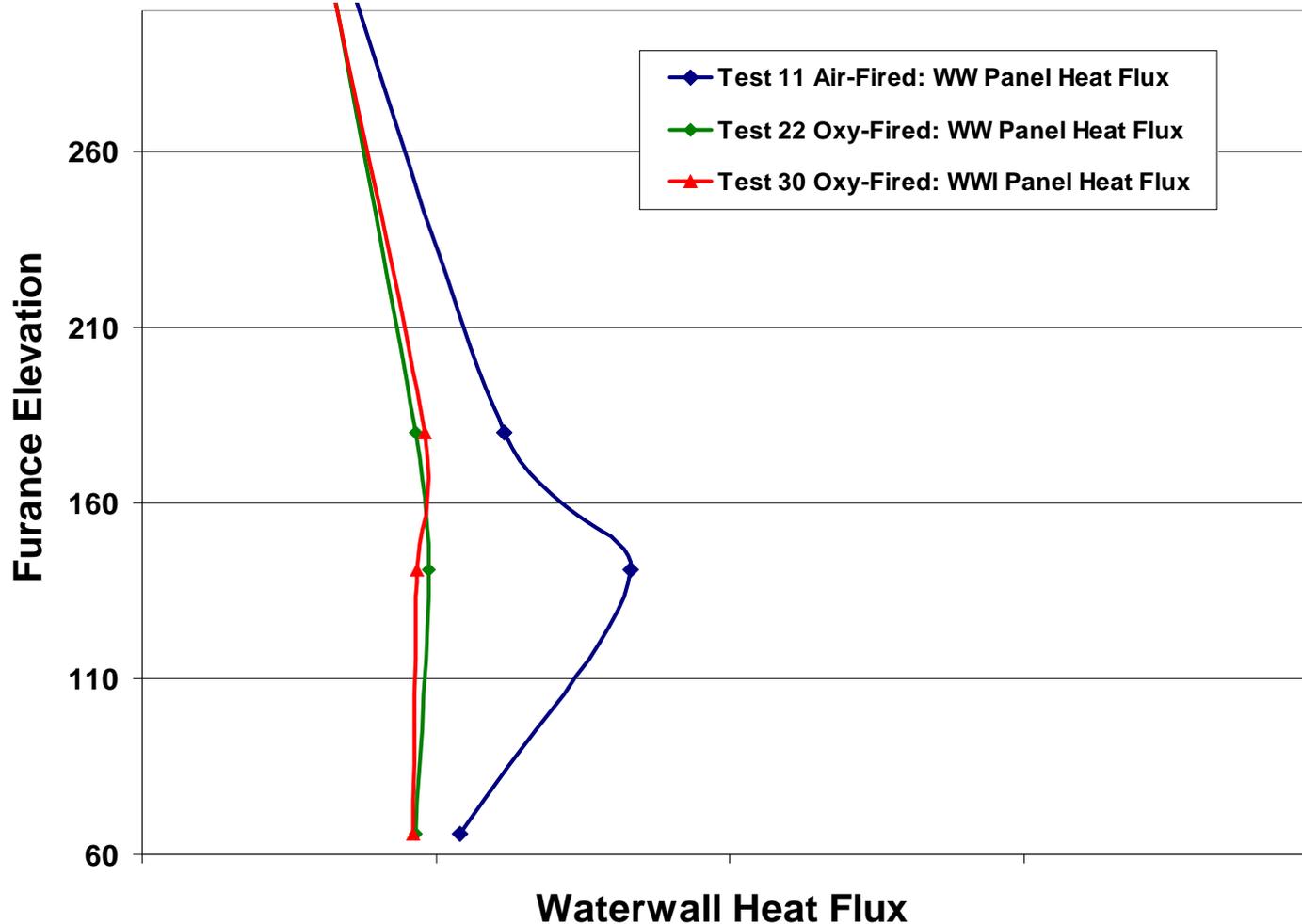
BSF Campaign 1 - PRB

Incident Heat Flux for Air-Firing vs. Oxy-Firing



BSF Campaign 1 - PRB

Waterwall Test Panel Heat Flux vs. Elevation

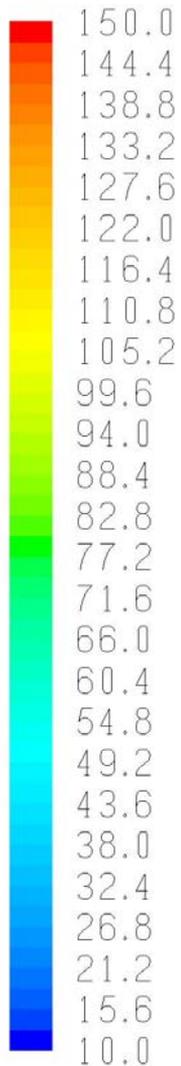


BSF Campaign 1 - PRB

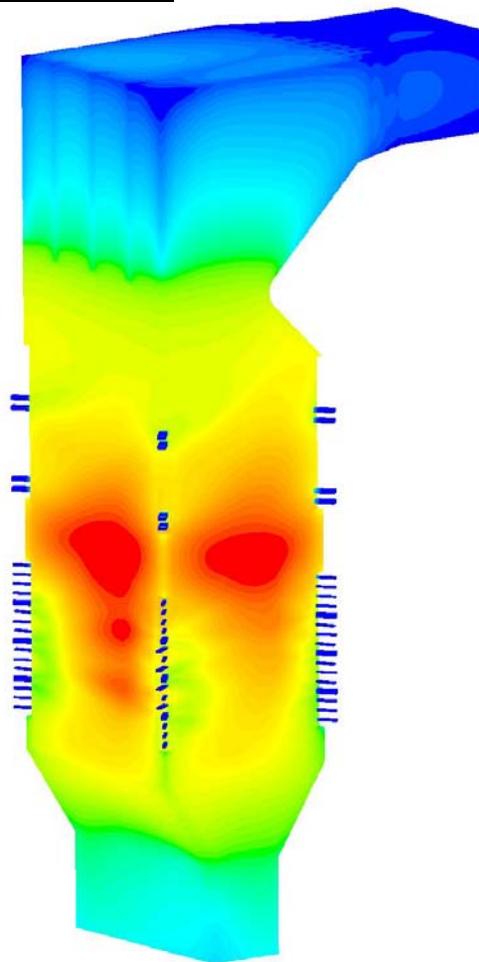
CFD Predictions of Wall Radiation



KBTU/hr-ft²

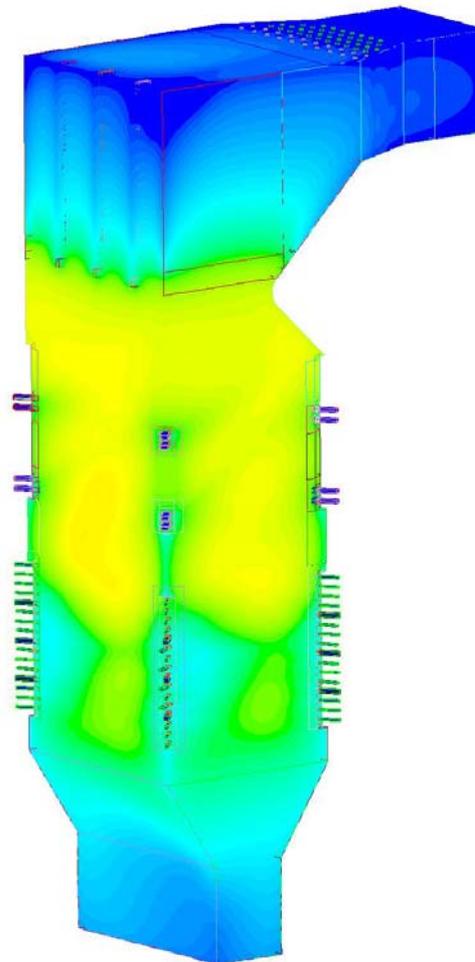


AIR Test 11



AIR

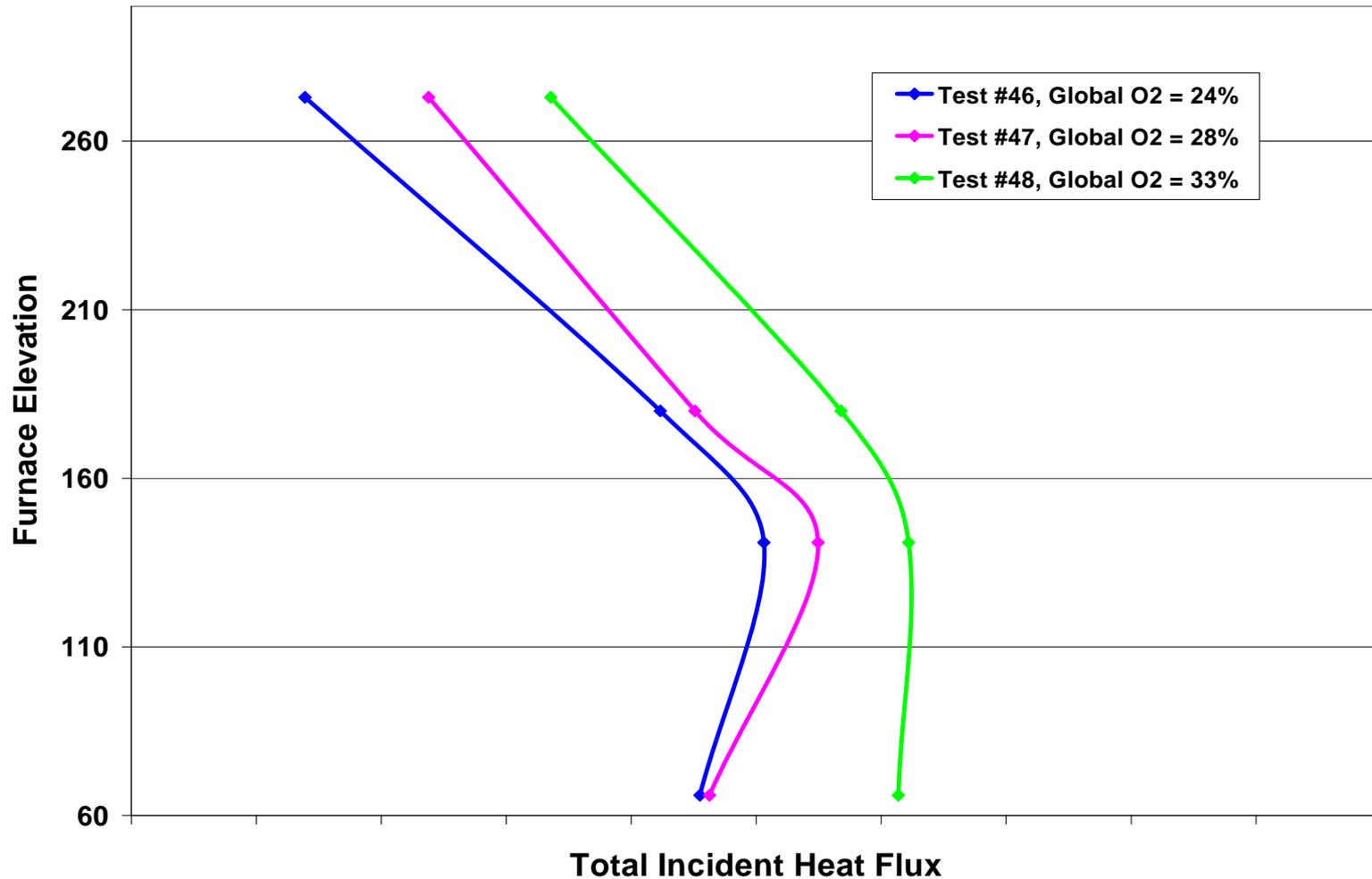
OXY Test 22



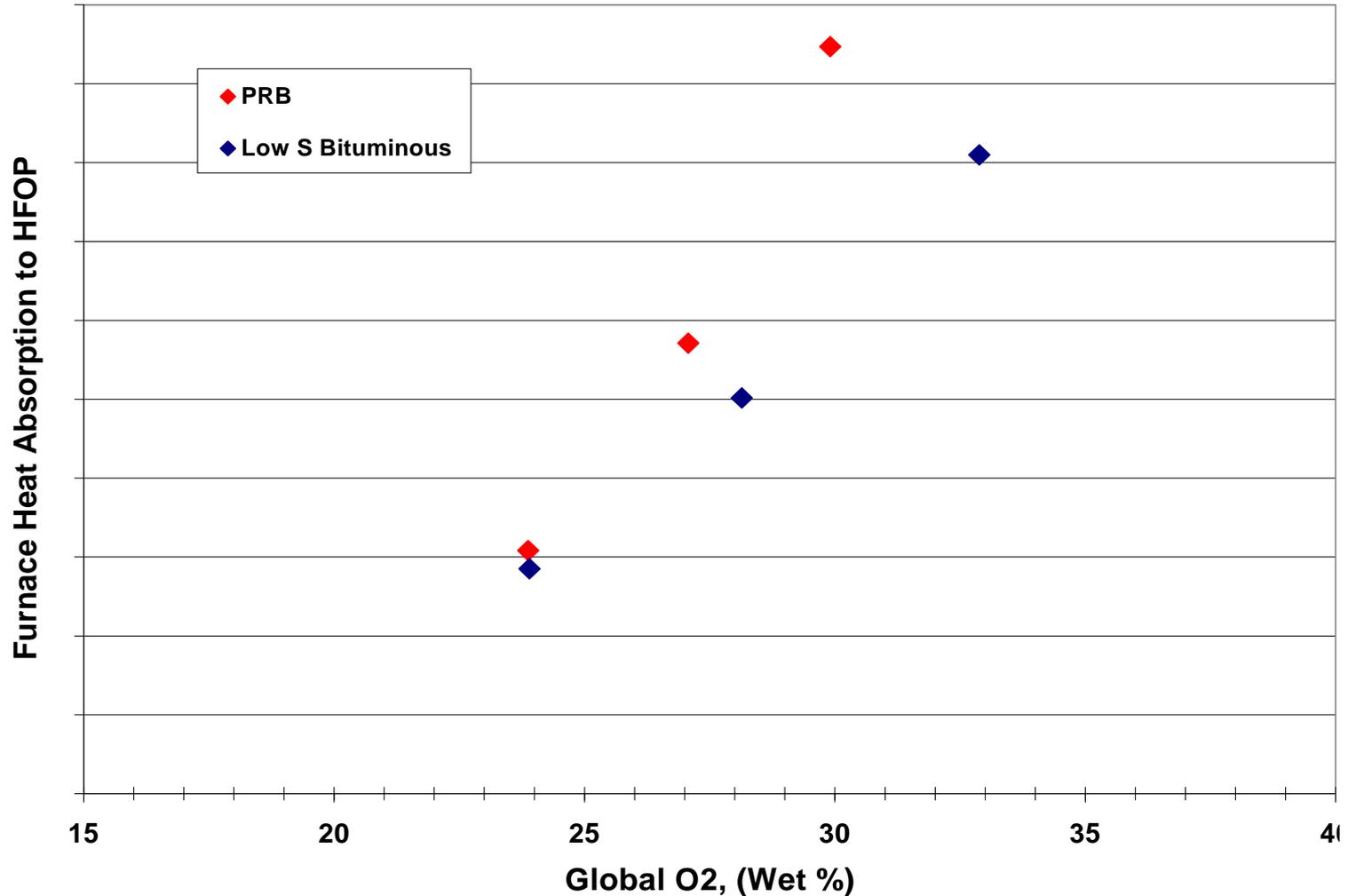
OXY



BSF Campaign 2 - Low S Bituminous Recycle Variations - Vertical Heat Transfer Profile



Impact of Gas Recycle – Lower Furnace Heat Absorption



BSF Campaign 2 - Low S Bituminous Incident Heat Flux for Air-Firing vs. Oxy-Firing



BSF Campaign 1 & 2 - General Observations **ALSTOM**

- **General Facility Operation**

- Stable operation over broad range of test conditions 
- Able to produce high (>90%) CO2 Flue Gas 

- **Combustion**

- Very good performance during both air and oxy testing with both PRB Sub and WV Bit Coals
 - Able to operate at low excess oxygen (Less than 2% O2 at Economizer Outlet) 
 - Low CO Emissions (near Zero) 
 - Low Carbon in Fly ash 

- **NOx Emissions**

- Lower NOx Emissions with Oxy-firing with both PRB Subbituminous and WV Bituminous) 
- Roughly 50% Reduction from Air-Firing on lb NOx / MMBtu Fired 

BSF Campaign 1 & 2 - General Observations **ALSTOM**

- **Heat Transfer**

- Generally similar range of heat flux and temperature 
- Able to change profile by adjusting operating conditions 

- **SO₃ Formation**

- SO₂ to SO₃ conversion appears to be similar 
- SO₃ concentrations about 3 times high for oxy-firing 

- **Ash Deposition**

- Appeared generally similar 
- Fly ash and lower furnace deposits had similar composition, upper furnace had higher sulfur content 

- **Waterwall Corrosion**

- Appeared generally similar 

Conclusions

- Major large oxy pilot projects are underway providing key technical information on
 - oxy firing impacts on boiler performance and operation
 - overall oxy plant integration and control.
- Pilot programs are providing design guidelines, performance data and validated tools.
- Pilot results along with other Alstom oxy projects, provide a strong foundation for the next step of demonstration (~250 MWe).
- Alstom is ready to take the next step of commercial scale demonstration



Thank You For Your Attention !

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