

# Recovery Act: Oxy-Combustion Technology Development For Industrial- Scale Boiler Applications DE NT-0005290

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NETL CO2 Capture Technology Conference  
Pittsburgh, PA  
August 24, 2011

POWER

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# The Alstom Group: A Worldwide Leader in Power Generation



- Clean Power



N°1 in integrated power plants



N°1 in air quality control systems

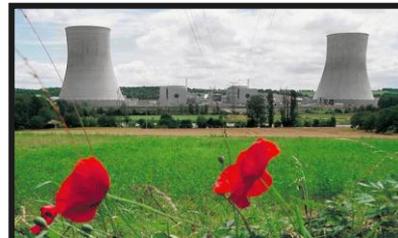


N°1 in services for electric utilities

- CO<sub>2</sub>-Free & Renewables



N°1 in hydro power



N°1 in conventional nuclear power island



Recent acquisition of solar and wind

- Carbon Capture

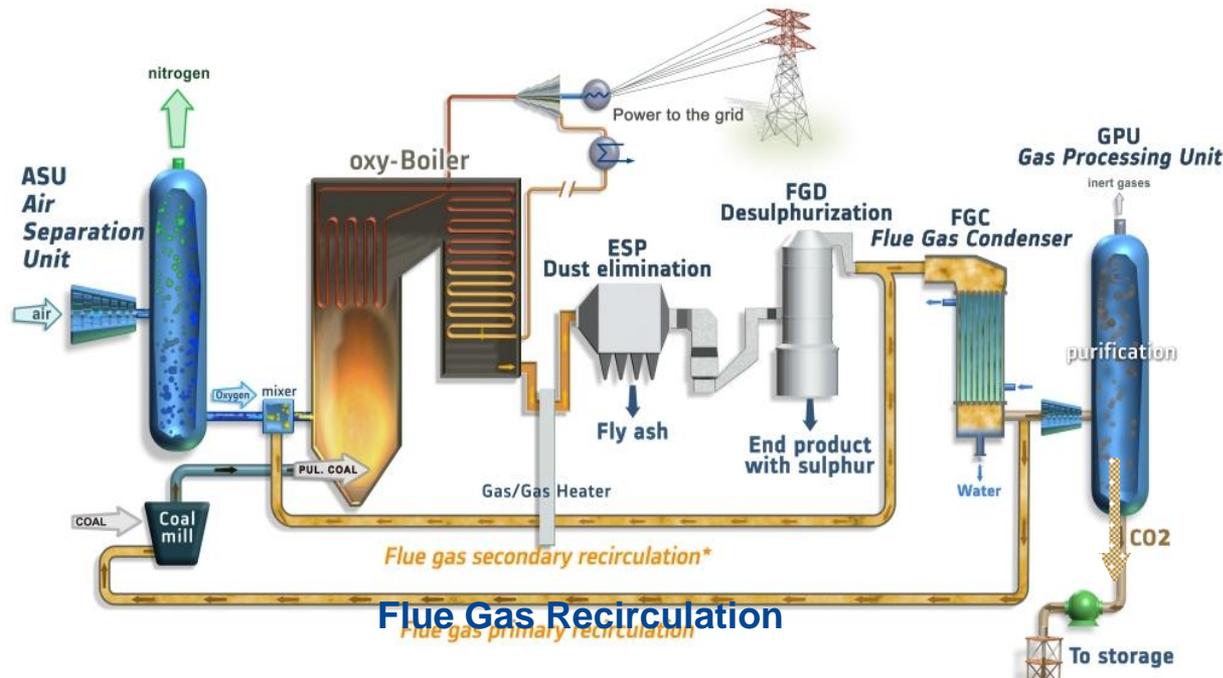
- Post-Combustion
- Oxy-Combustion



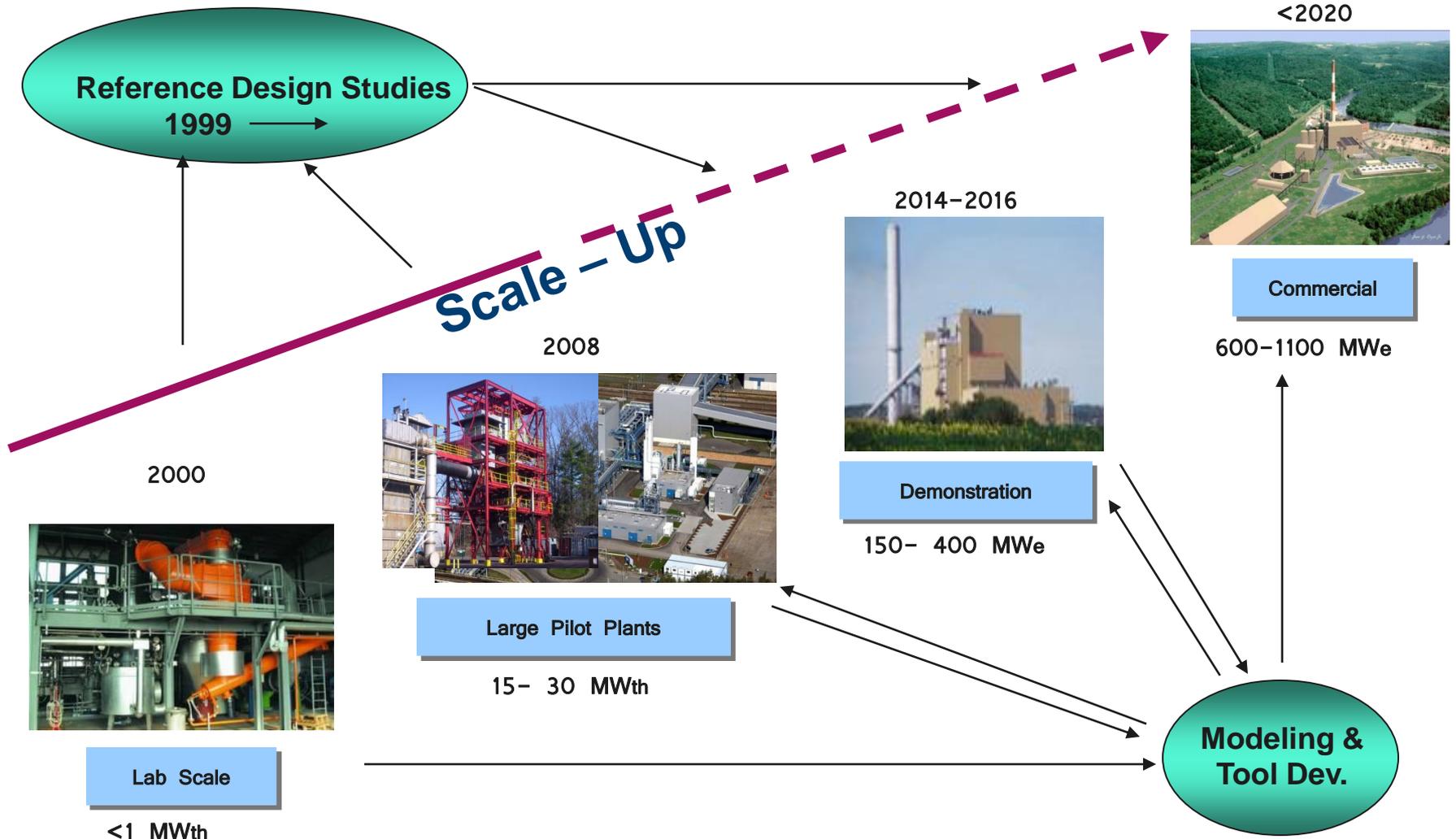
## Full Power Systems Portfolio and Technology Mix

# Oxy-Combustion Technology - Why Oxy?

- Cost Competitive (with other CCS, Wind, Solar, Biomass)
- Reliability / Low Risk: Adapts Conventional Components
- New and Retrofit Applications
- High CO<sub>2</sub> Capture Rates (>90%)
- Near Zero Emissions
- CO<sub>2</sub> “Ready” Approach
- Potential for O<sub>2</sub> Production Cost Reduction



# Alstom Oxy-PC Combustion Technology Development Steps



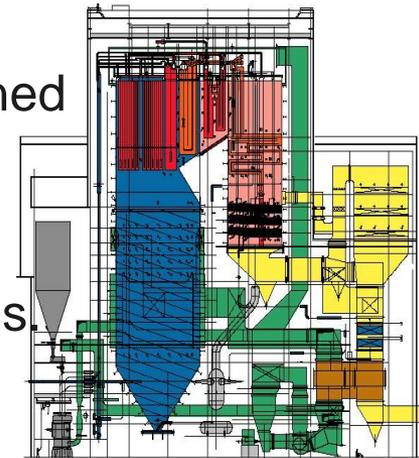
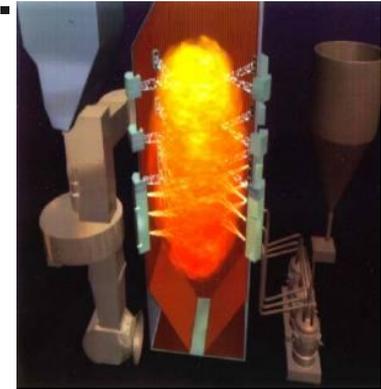
# Oxy T-Fired Boiler Development

## Project Objectives



**Develop and validate an oxyfuel T-fired boiler system as part of commercially attractive CO<sub>2</sub> capture solutions.**

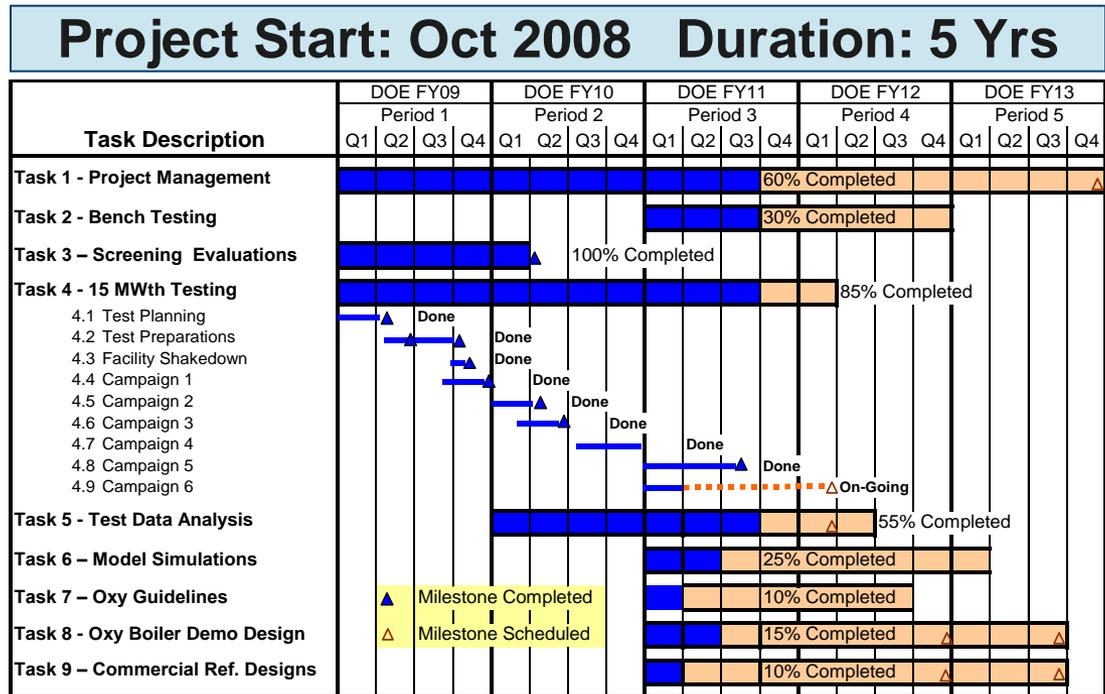
- Design and develop an oxyfuel firing system for T- fired boilers
- Evaluate the performance in pilot scale tests at 15 MW<sub>th</sub> testing
  - operation, combustion, heat transfer, pollutants, ash deposition and corrosion
- Evaluate and improve engineering and simulation tools for oxy-combustion by applying detailed test data obtained
- Develop design guidelines
- Develop the design, performance and costs for a demonstration-scale oxyfuel boiler and auxiliary systems
- Develop the design and costs for both industrial and utility commercial-scale reference oxyfuel boilers



# Oxy T-Fired Boiler Development Budget & Schedule



**Total Budget: \$21.5 M**  
**DOE Funding: \$15.0 M**  
**Other Funding: Alstom, ICCI, NDIC, Utilities**



## Utility Advisory Group

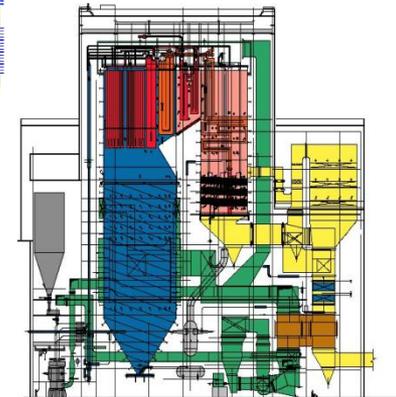
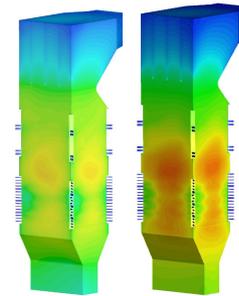
- Ameren
- ATCO
- Dominion Energy
- Great River Energy
- Luminant (TXU)
- LCRA and Austin Energy
- MidWest Generation
- NB Power
- OG&E
- Vattenfall



# Project Status

## Accomplished

- Process and CFD Screening Completed
- Modifications For Oxy-Firing Completed
- Campaign 1 Testing Completed Sept. 2009 – Subbituminous coal
- Campaign 2 Testing Completed Feb. 2010 - Low S Bituminous coal
- Campaign 3 Testing Completed April 2010 - High S Illinois Bituminous coal
- Campaign 4 Testing Completed Oct. 2010 - North Dakota Lignite
- Campaign 5 Testing Completed August 2011- Schwarze Pumpe Lignite



## Next

- Campaign 6 Testing of 2<sup>nd</sup> Generation Concepts
- Tools & Modeling Refinement and Validation on-going
- Design guidelines On-going
- Reference & Demo designs On-going

# 15 MWth Oxyfuel Pilot Plant: Alstom Boiler Laboratories, Windsor, CT



## 15 MWth Boiler Simulation Facility -

Multi-burner, Tangentially-fired

## Flexible operating conditions

- air & oxy-firing, gas recycle configuration, oxygen injection, firing system design

## Generation of detailed design and performance data

- combustion, emissions, heat transfer, deposition, corrosion



# Oxy-PC Boiler

## Development areas investigated



	<b>Evaluated Under Pilot-Scale Testing</b>
	<b>Evaluated Under Design Studies</b>

Operation/load change:  
dynamic response

Heat transfer :  
radiative / convective

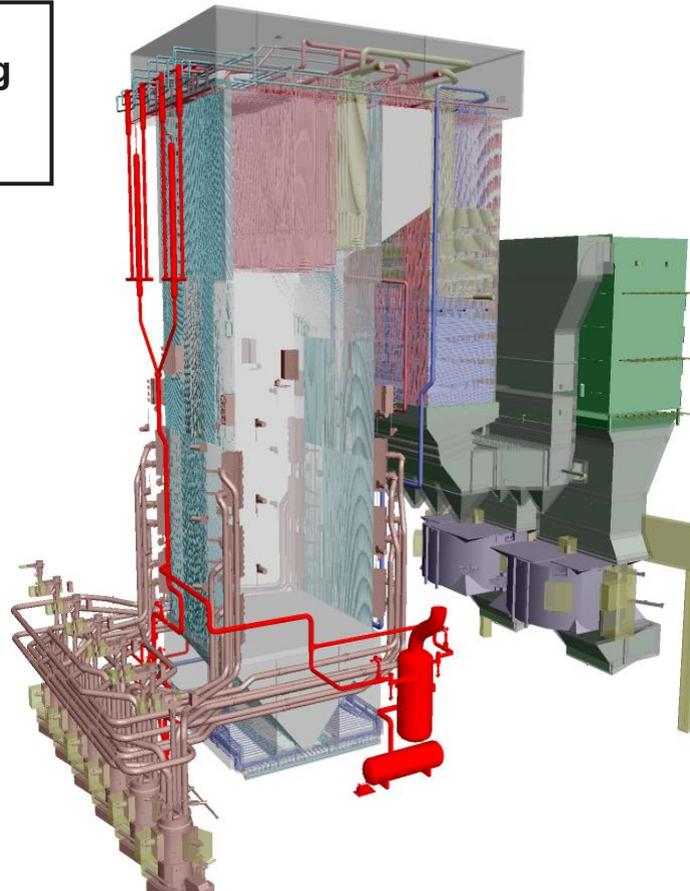
Oxy tangential firing system  
design

Oxygen Injection

Effect of coal quality

Flue gas recycle

Mill adaptation / integration



Control Logics & Safety

Corrosion  
- high temperature  
- low temperature

Fouling & Slagging

SCR adaptation

Air in-leakage

Gas pre-heater adaptation

Acid dew point

Excess O<sub>2</sub>

Emissions

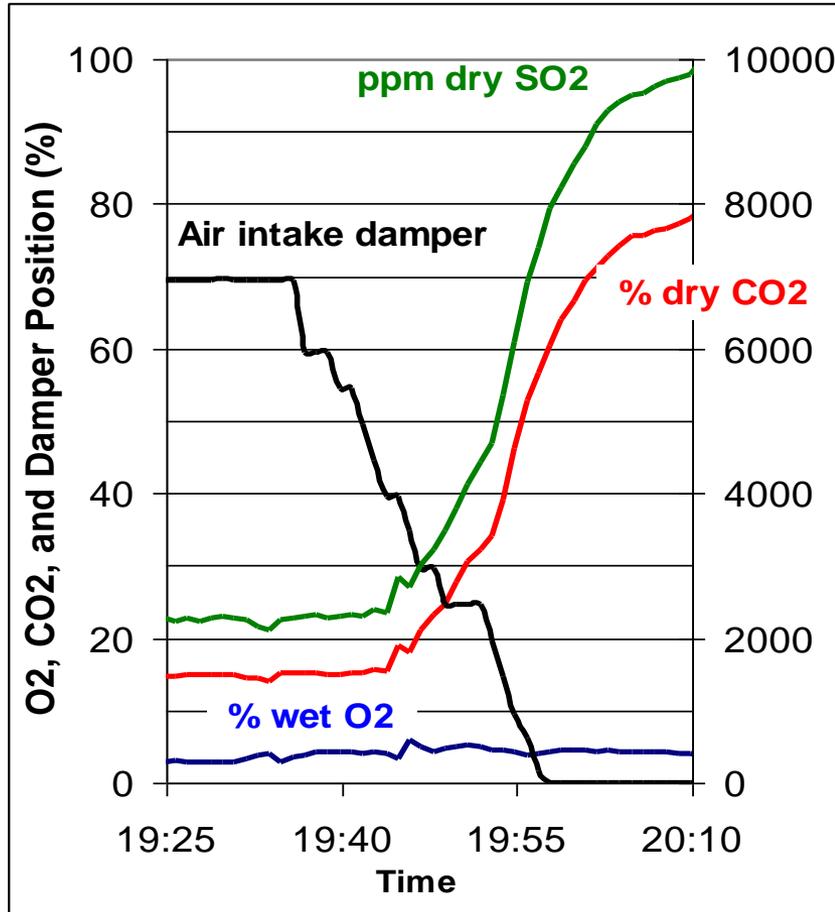
Ash Properties

**Comprehensive Test Program Addresses Several Areas**

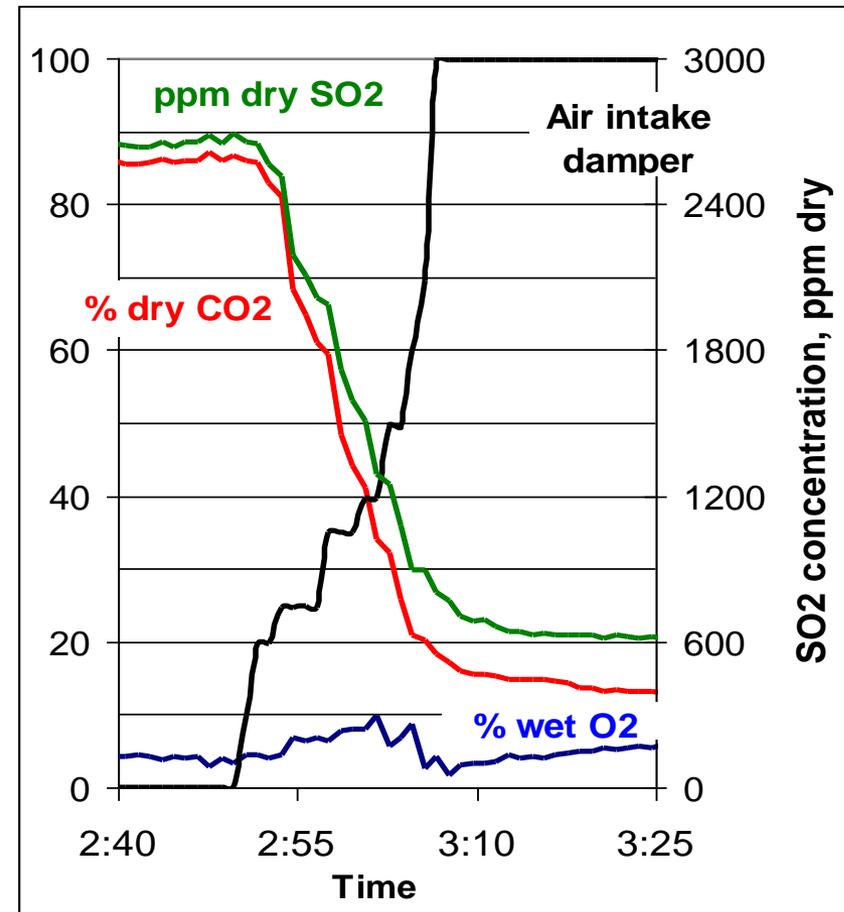
# 15 MWth Oxyfuel Pilot Plant: Switch from air to oxy firing demonstrated



## Air to Oxy Transition

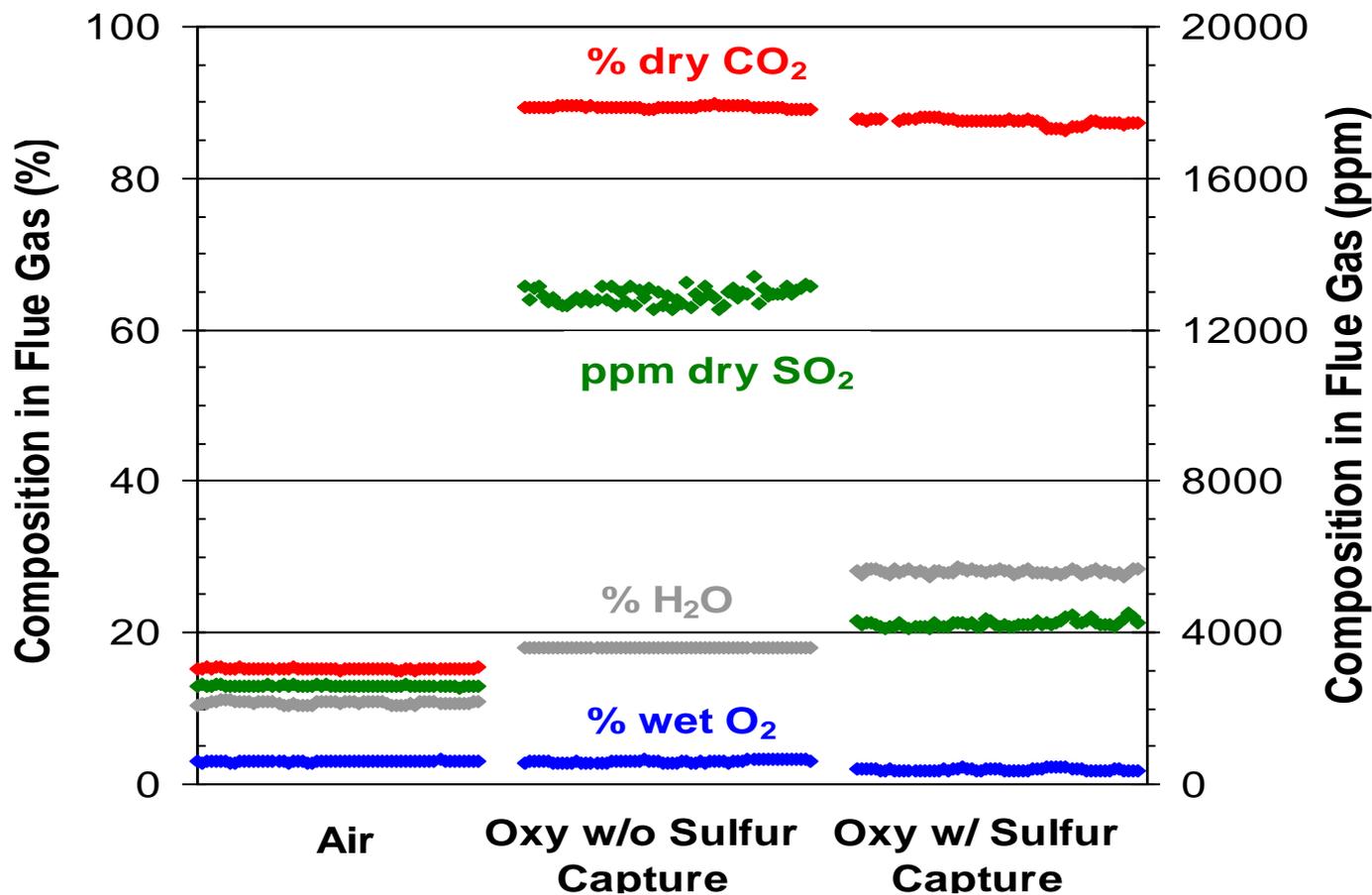


## Oxy to Air Transition



**Transitions Air-to-Oxy or Oxy-to-Air about 30 mins**

# Changes in Oxy-Firing Gas Compositions – Illinois High Sulfur Coal

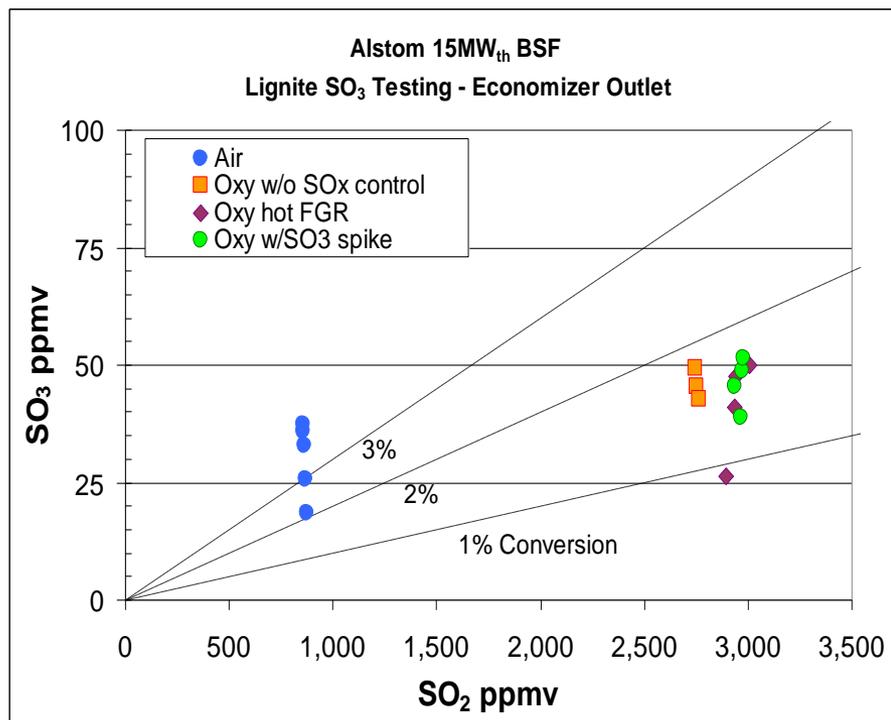


**Significant Increase in SO<sub>2</sub> even with sulfur capture**

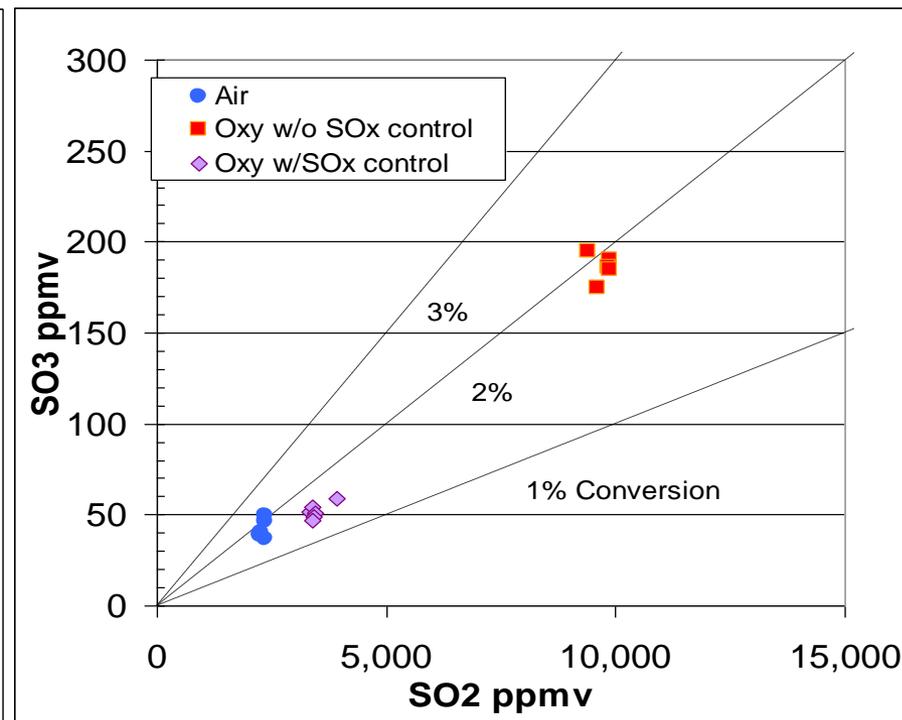
# Similar SO<sub>3</sub> Conversion Rate As Air Firing - Economizer Outlet Measurements in BSF



North Dakota  
Economizer Outlet SO<sub>3</sub> results



Illinois Bituminous  
Economizer Outlet SO<sub>3</sub> results

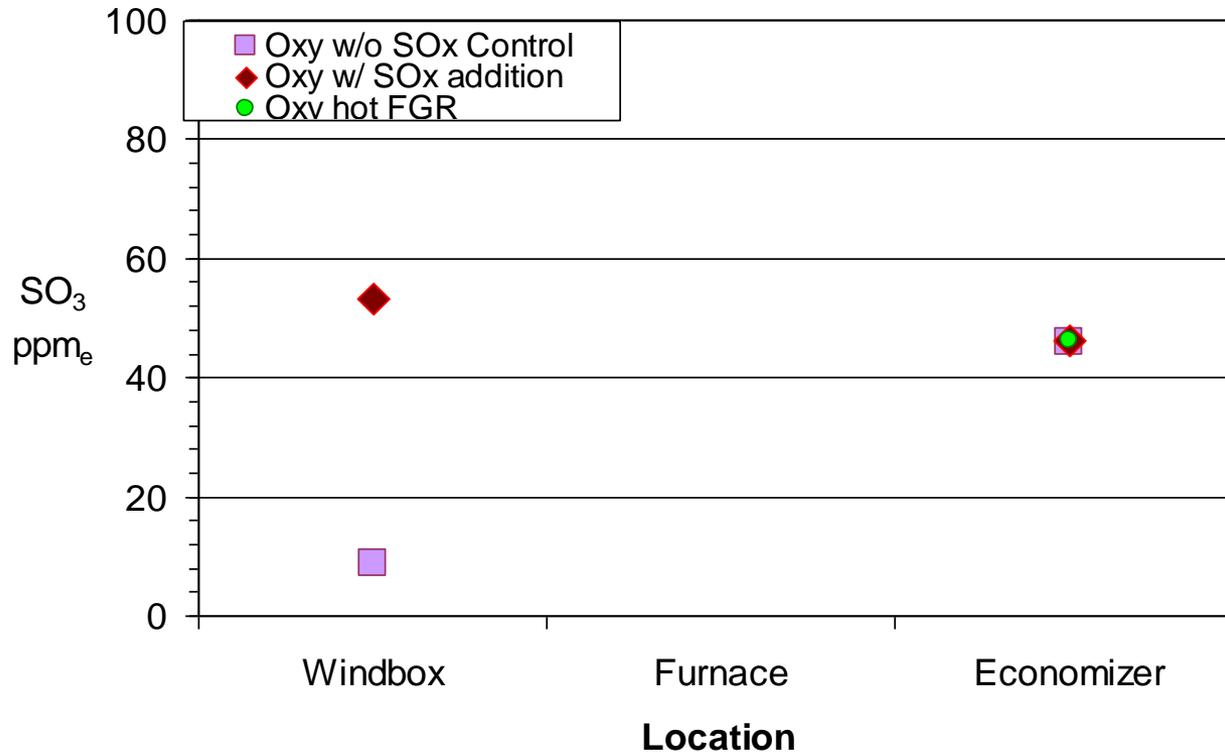


**Similar SO<sub>2</sub> to SO<sub>3</sub> conversion rates**

# Conversion Checked By SO<sub>3</sub> Addition: SO<sub>3</sub> Measurements Along System Path



Alstom 15MWth BSF  
Lignite SO<sub>3</sub> Testing



For windbox ppm<sub>e</sub> is the equivalent ppm impact @ the economizer outlet

$$ppm_e \equiv ppm \cdot \frac{\dot{n}_{SecondaryFGR}}{\dot{n}_{FurnaceOut}}$$

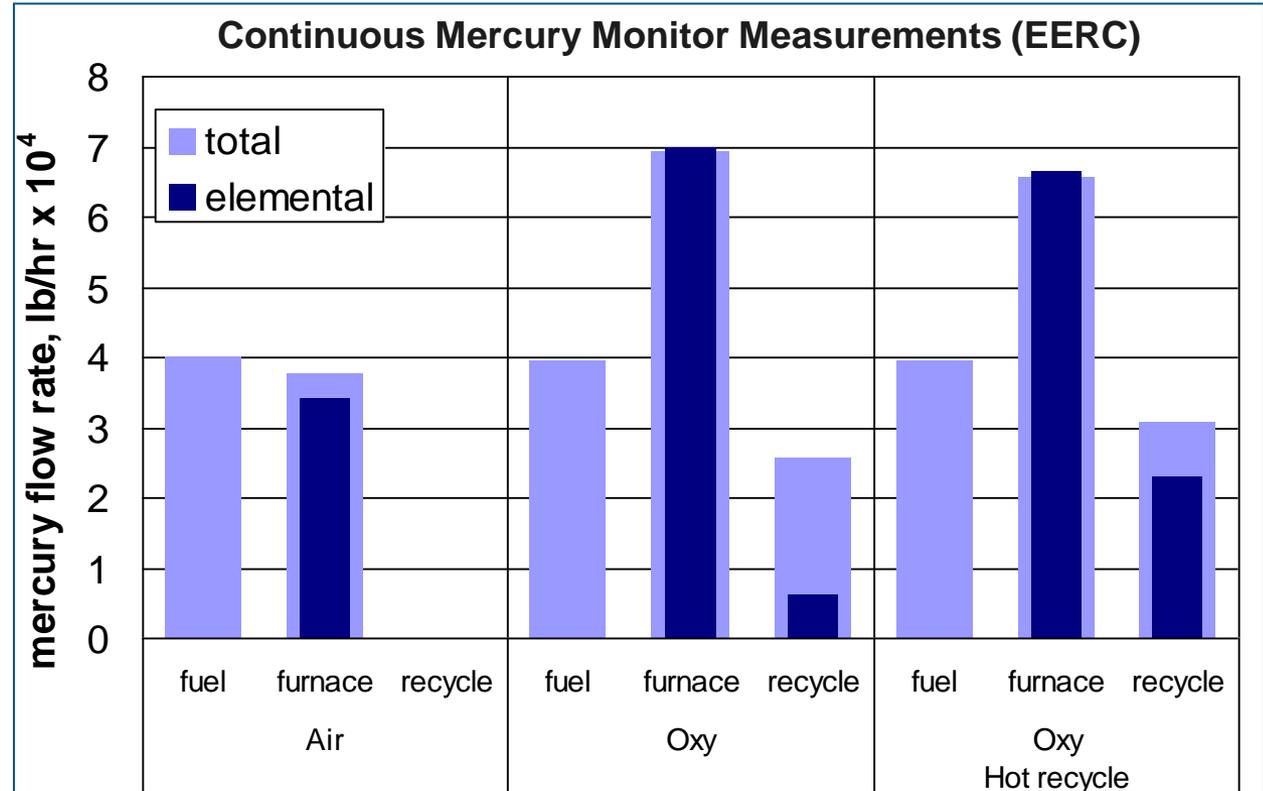
**Recycled SO<sub>3</sub> does not impact outlet emissions**

# Mercury Measurements -15 MWt North Dakota Lignite Testing



## Mercury Measurements (Total and Speciation)

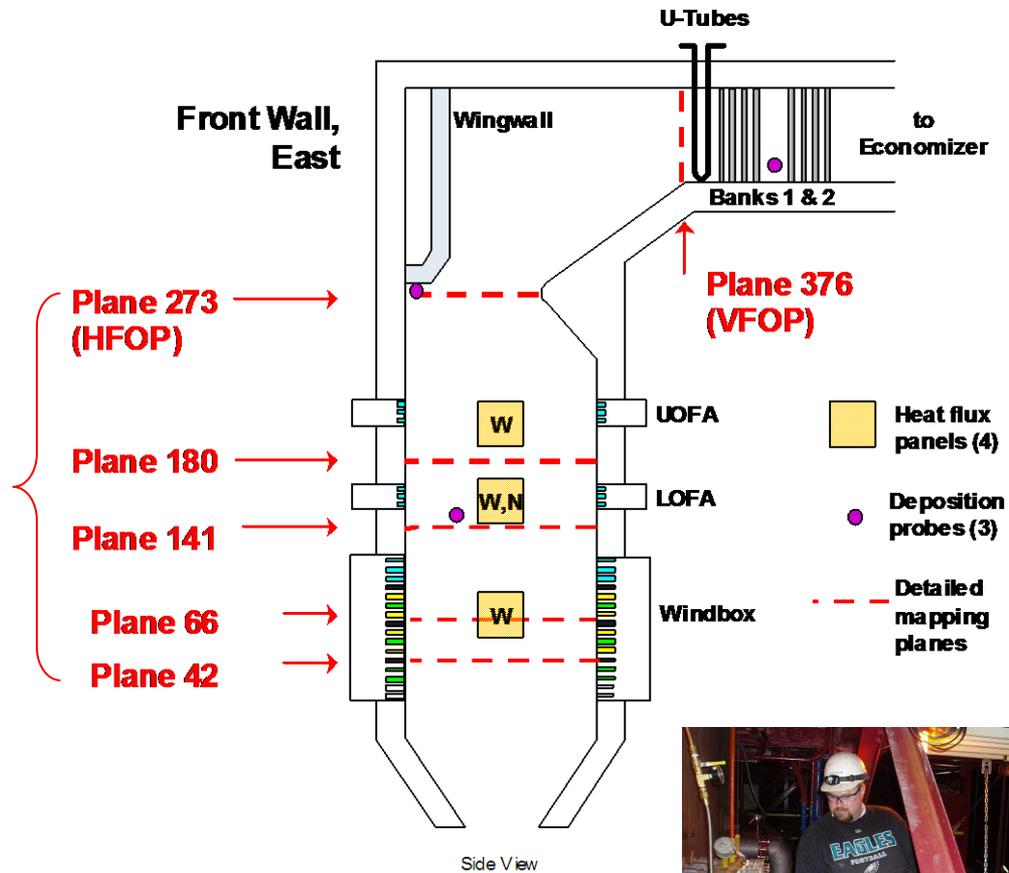
- Continuous Mercury Monitors (Tekran)
- Sorbent Traps
- Ontario Hydro



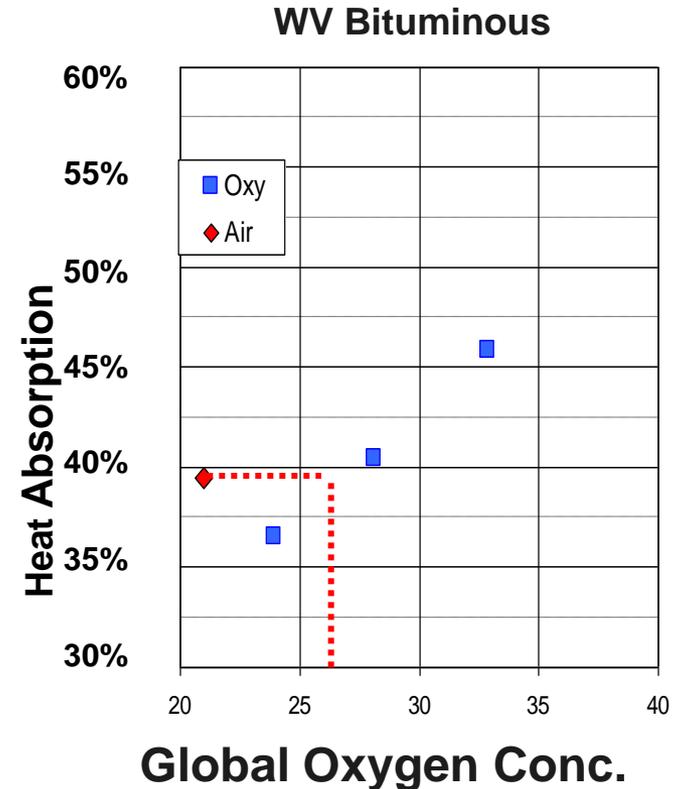
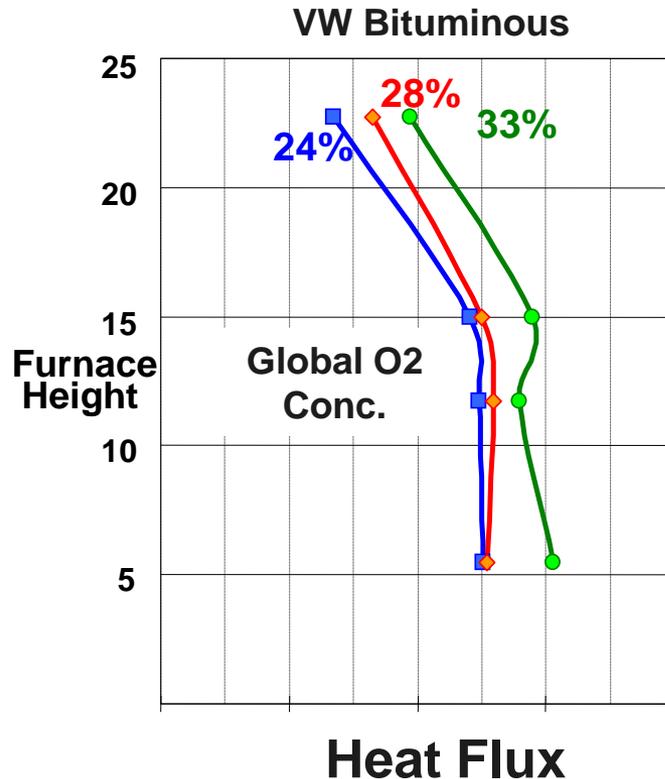
Mercury levels increase during oxy-firing at economizer outlet  
Net mercury loadings leaving the boiler system similar to air

# 15 MW<sub>th</sub> BSF furnace mapping

Probe Mapping Measurements
<b>Gas Temperatures</b>
<b>Heat Flux:</b>
- Total Incident
- Radiant
<b>Gas Species:</b>
- O <sub>2</sub>
- CO
- CO <sub>2</sub>
- SO <sub>2</sub>
- H <sub>2</sub> O
- TCH

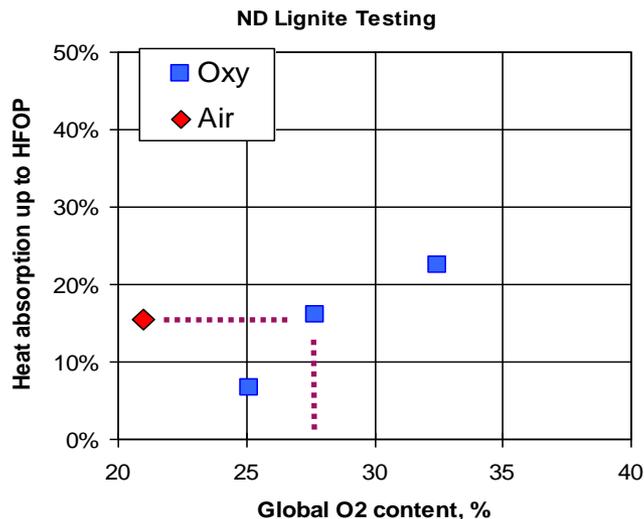
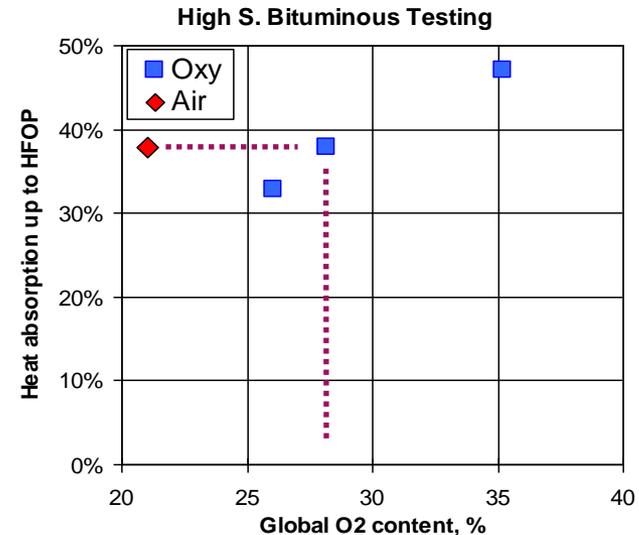
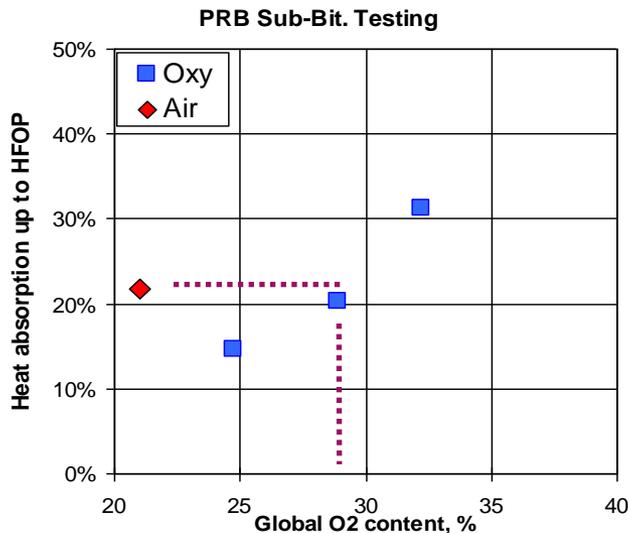


# Furnace WW heat flux – gas recycle rate impacts



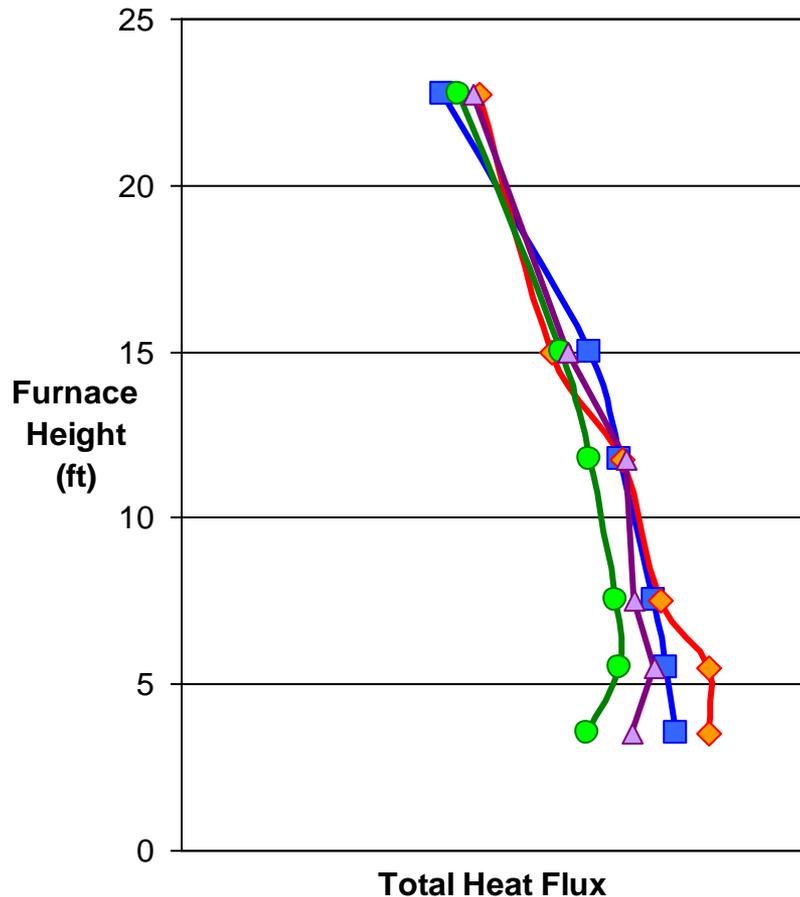
Ability to control heat flux magnitude with recycle rate  
 Reduced recycle rate shifts heat duty to furnace

# A reduced recycle rate shifts more heat absorption to the furnace



**In each case, a global O<sub>2</sub> of ~26 - 28% gives the same furnace absorption as air firing in the BSF**

# The heat flux profile can also be controlled by adjusting the O<sub>2</sub> injection



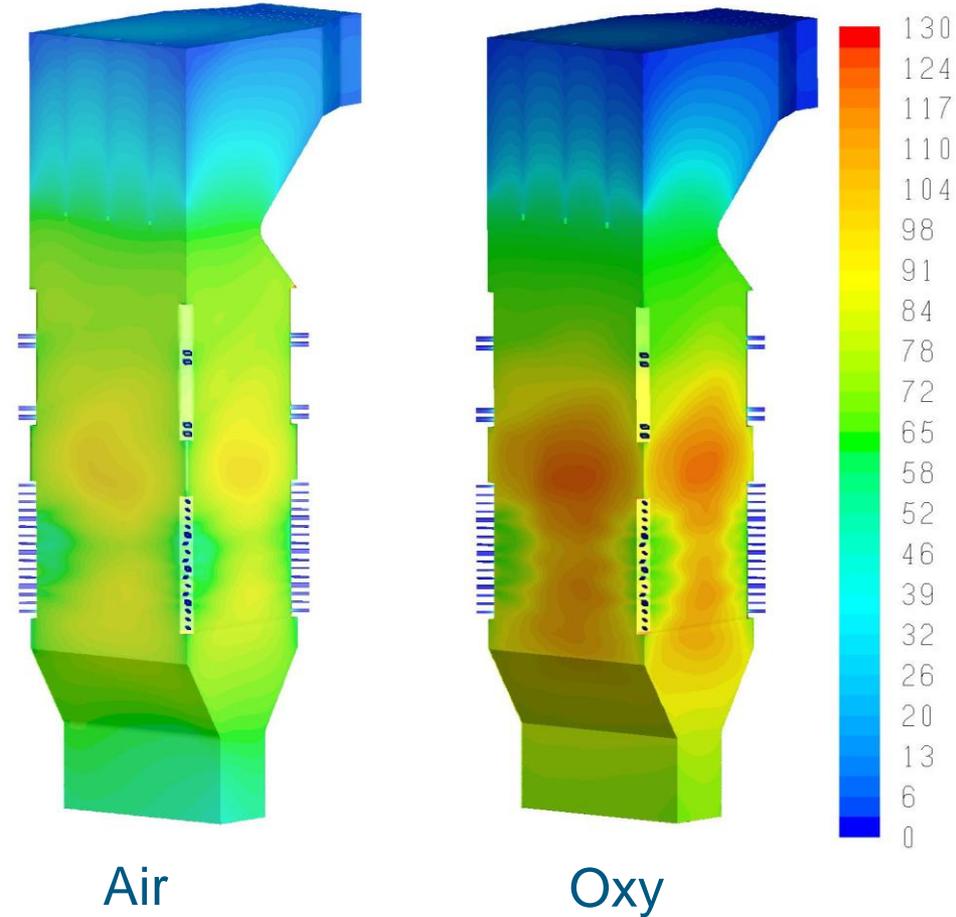
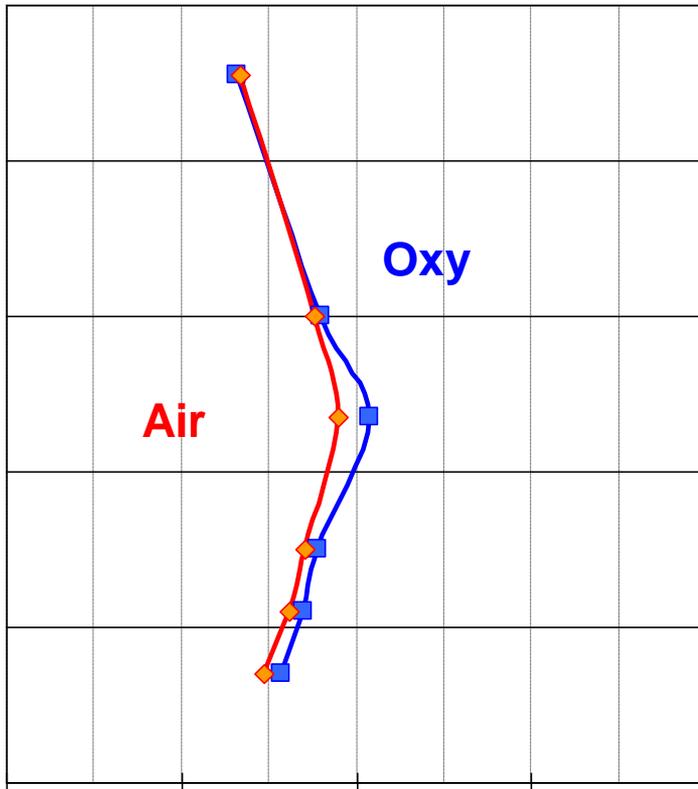
Furnace heat flux changed with oxygen flow rate and concentration

- Oxygen was varied between the overfire and windbox locations
- Oxygen was varied among the different windbox compartments

High-S bituminous

# The oxy-fired heat flux profile can be controlled to match the air fired

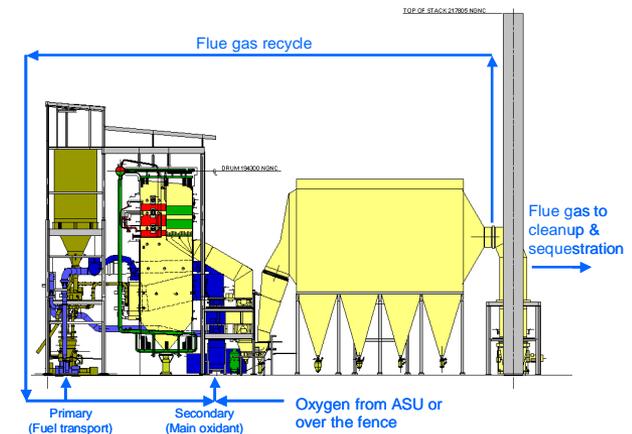
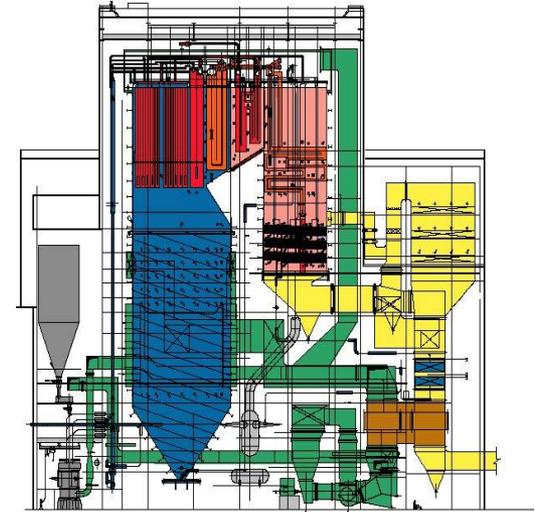
Alstom 15MW<sub>th</sub> BSF  
ND Lignite Long-Term Testing



# Oxy T-Fired Boiler Design

## Oxy Demonstration and Reference Boiler Design Packages

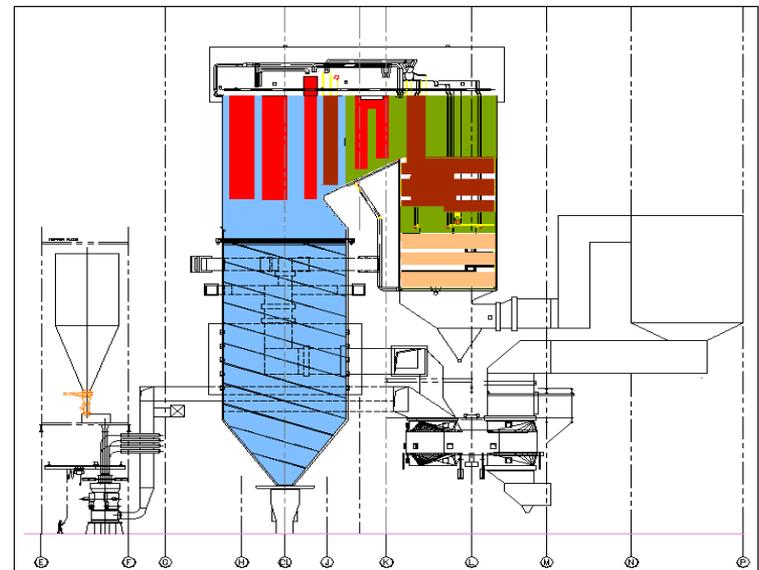
- Application of test results and design tools
- Development of a full-scale oxy-fired boiler design for demonstration
- Development of reference oxy-fired utility boiler design for future market
- Development of reference oxy-fired boiler design for industrial application
- Detailed design, performance assessment and costing for entire boiler island to the level needed for firm bid sale



# Oxy-fired Boiler Demonstration Design



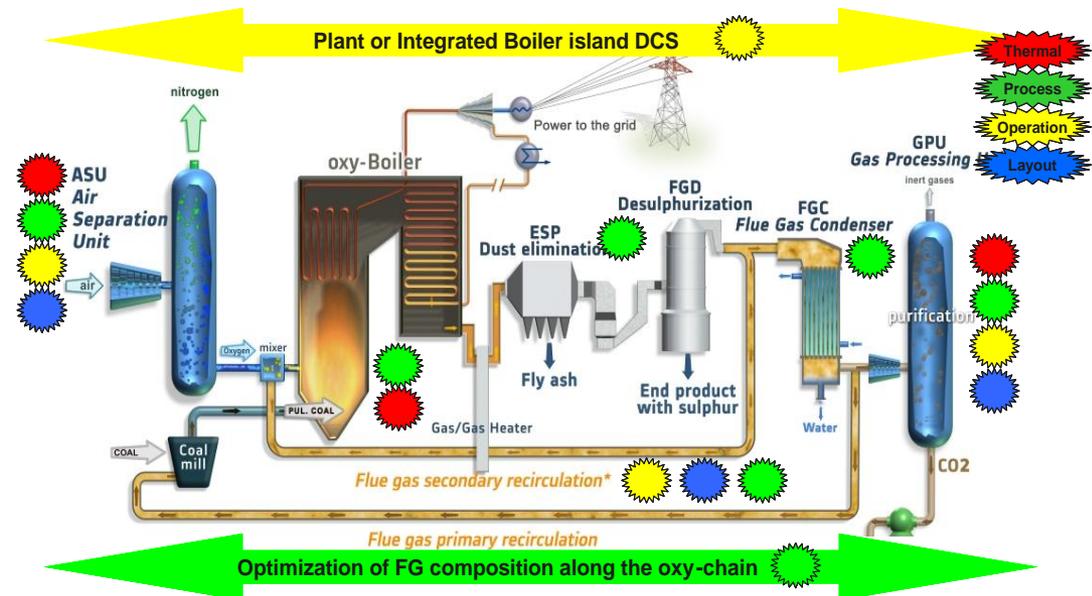
- Developed specifications for 400 MWe supercritical design (low sulfur bituminous design coal)
- Phase 1 develops oxy-fired design that retains air-firing capability. (Addresses retrofit case).
- Phase 2 develops oxy-fired design with advanced supercritical steam cycle optimized for oxy-firing. Including assessment of trade-offs
  - materials
  - pressure part arrangement
  - recycle configuration
  - overall plant cost & performance



# Oxy-fired Reference Designs

- Developed specifications for 900 MWe advanced supercritical design (low sulfur bituminous coal)
- Preliminary specifications for reference industrial design for co-generation unit firing coal and biomass (equivalent steam generation ~150 MWe)
- Oxy-fired design optimized globally for plant performance and cost of electricity

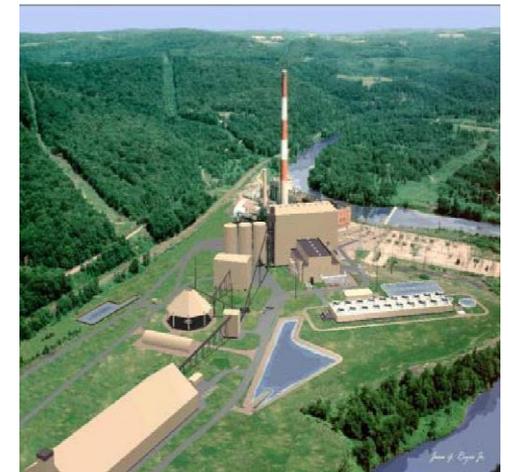
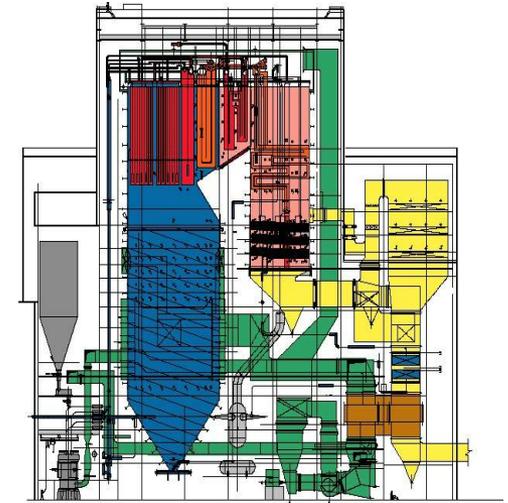
- Integration (process, heat, arrangement, operation)
- Balance trade-offs between main subsystems (performance and costs)



- No technical barriers that would restrict the continued development and commercialization of oxy-combustion
- Combustion performance, emissions, and thermal behavior (temperature, heat flux intensity, heat flux profile) can be controlled to similar levels as air firing.
- An oxy tangentially-fired boiler does not require major changes to current boiler design.
  - For oxy-combustion retrofit, boiler size and pressure part surfaces should only require minor design modifications.
  - For new applications, additional control under oxy-firing may be used to an advantage with innovative design concepts to improve oxy-fired boiler performance and costs.

# Concluding Remarks

- Detailed test data from this project and other Alstom R&D programs is being applied to
  - refine and validate design tools and design procedures.
  - support overall oxy plant integration and optimization efforts
  - develop and optimize designs for demonstration opportunities and future commercial plants



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