

# ALSTOM's Chemical Looping Combustion Prototype for CO<sub>2</sub> Capture from Existing Pulverized Coal Fired Power Plants

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2011 CO<sub>2</sub> Capture Technology Meeting , August 22 – 26, 2011



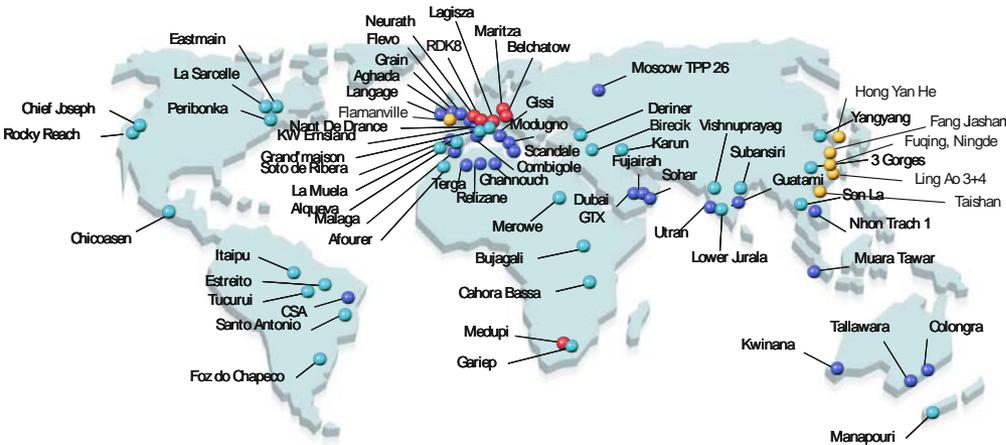
Topic 1            General Project & Technology Background

Topic 2            Phase 0 to III Activities

Topic 3            Phase IV Activities and Status

Topic 4            Next Steps

# The Alstom Group: a Worldwide Leader in Power Generation



Over 41 GW under execution

- Nuclear
- Hydro
- Steam
- Gas

**Chemical Looping  
Technology Development**

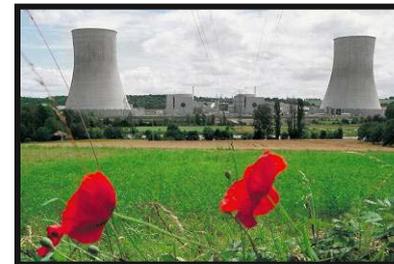
**Full Power Systems Portfolio**



N°1 in hydro power



N°1 in integrated power plants



N°1 in conventional nuclear power island



Recent acquisitions of solar & wind power



N°1 in air quality control systems



N°1 in services for electric utilities

## Project Goals and Objectives

- Chemical Looping Program:
  - Develop and commercialize chemical looping process to meet the goals for existing or new coal-fired power plants.
- Prototype Project:
  - Design (BP1), build, and test (BP2) a 3 MWth Prototype to demonstrate Chemical Looping (40hr auto-thermal operation).
  - Obtain engineering and operating information necessary to design and build a reliable follow-on demonstration plant.

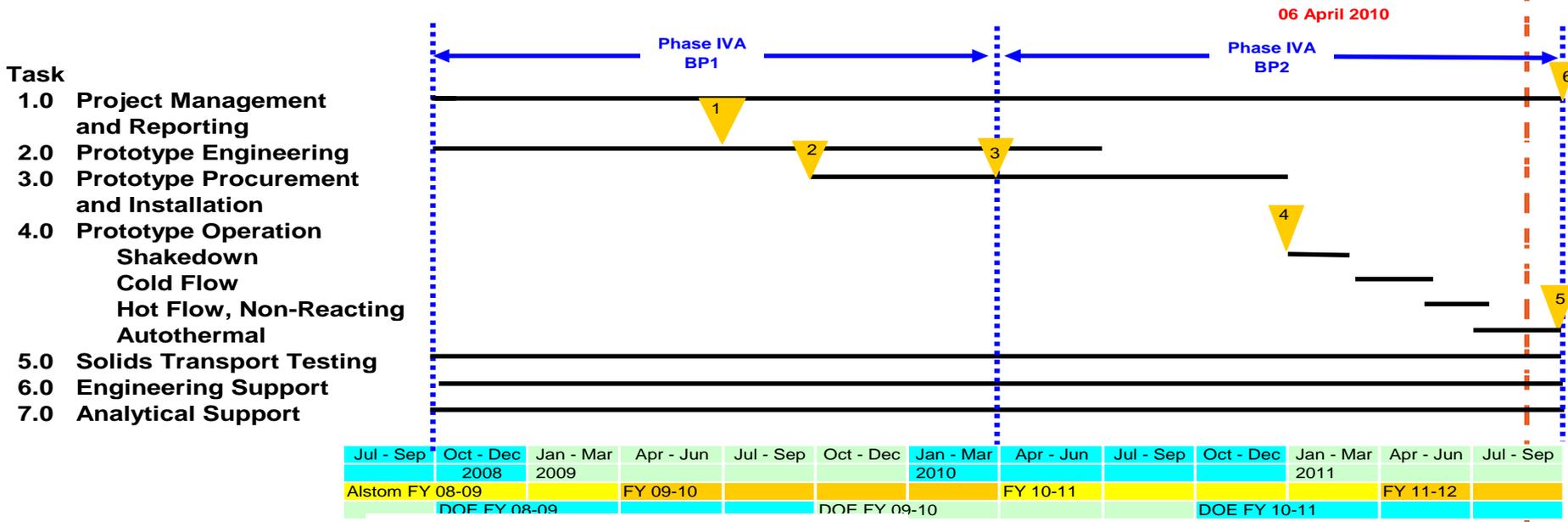
## Targets:

- Over 90% CO<sub>2</sub> capture from coal
- Less than \$20/ton avoided cost of CO<sub>2</sub> capture
- Capital cost 20% < conventional steam plant (w/o CO<sub>2</sub> capture)
- Applicable to retrofit and new coal-fired power plants
- Retrofit < 20% increase in COE
- Beat steam power and IGCC performance and economics, world-wide
- Medium-Btu gas or hydrogen without oxygen plant
- Economical H<sub>2</sub> production at low cost

# Chemical Looping Prototype Schedule As Planned



## Phase IVA DOE Schedule



### Milestones:

- |   |                                      |
|---|--------------------------------------|
| <b>1.</b> Complete Preliminary Engineering  | <b>4.</b> Start Shakedown            |
| <b>2.</b> Deliver Updated Technical and Cost Information to NETL (for BP1 Decision) | <b>5.</b> Complete Phase IVA Testing |
| <b>3.</b> Start Installation  | <b>6.</b> Deliver Interim Report     |
|   | <b>7.</b> Deliver Final Report       |

Phase IVA is on Schedule

## **Total Budget Period 1 & 2**

DOE Funding	\$6,895,624
Alstom Funding	\$1,723,906
<b>Total Budget</b>	<b>\$8,619,530</b>

### Participants:

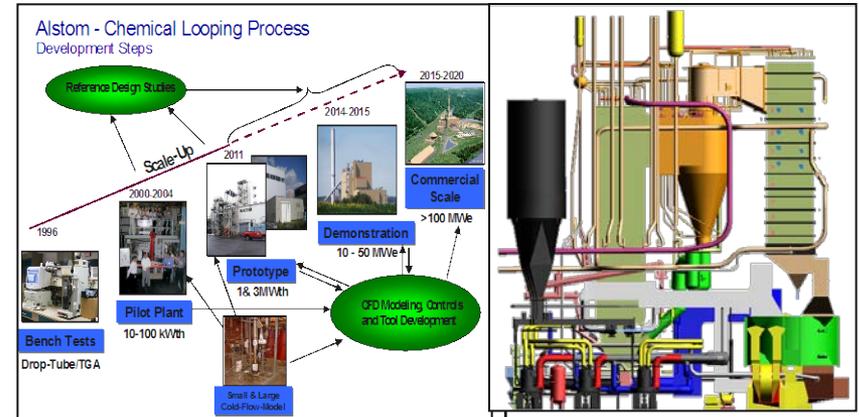
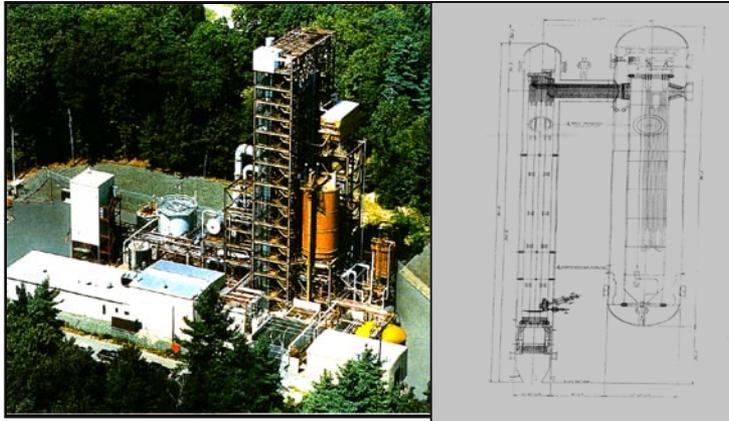


# Alstom's Limestone Chemical Looping Concept Evolution



## Alstom Entrained Gasification Technology (1974 – 1981)

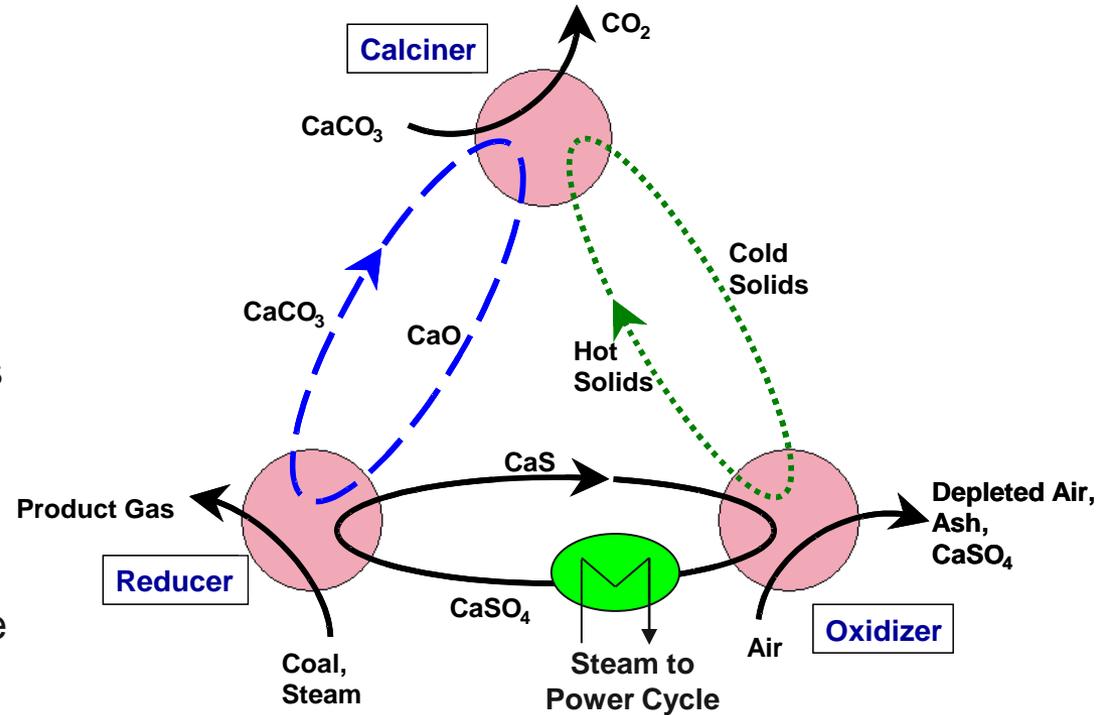
## Alstom Fluidized bed Technology (1978 - )



# Alstom's Limestone Based Chemical Looping Technology

# Alstom's Limestone Chemical Looping Concept

- In Alstom's process, calcium compounds from limestone are used as the reactant
- Coal is indirectly combusted or gasified by hot oxygen carrying reactant
- The Reactant is not consumed and is alternately reduced (oxygen removed) and oxidized (oxygen replenished) as it cycles between reactors
- The Reactant also carries heat where needed



## Main Reactions:

### Air Reactor (Oxidizer)

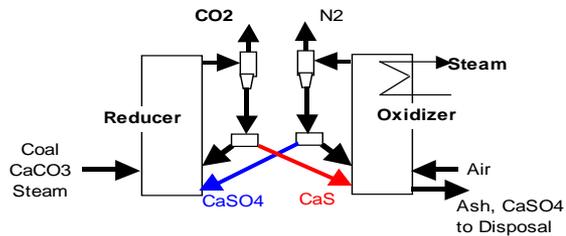


### Fuel Reactor (Reducer)

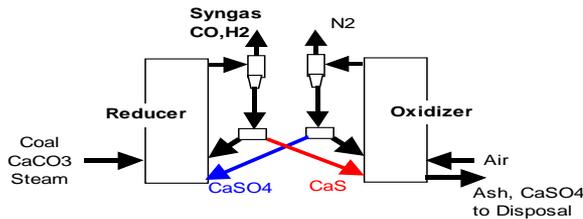


## Alstom's Limestone-based CLC Process

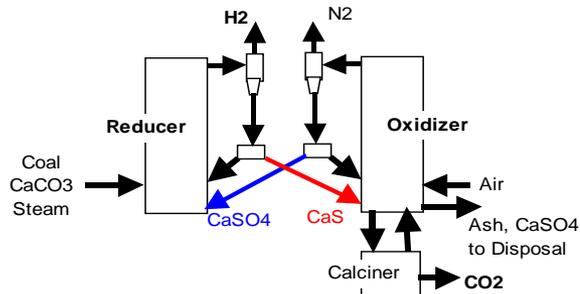
# Chemical Looping Process: Options and Applications



**Option 1 – Combustion with CO<sub>2</sub> Capture**



**Option 2 – Syngas with no CO<sub>2</sub> Capture**



**Option 3 – Hydrogen with CO<sub>2</sub> Capture**

## Applications

- CO<sub>2</sub> Capture – PC Retrofit
- CO<sub>2</sub> Capture – CFB Retrofit
- CO<sub>2</sub> Capture-Ready Power Plant
- Advanced Steam Cycles with CO<sub>2</sub> capture

- IGCC with Down-Stream CO<sub>2</sub> Capture
- Industrial Syngas production
- Coal-to-Liquid Fuels

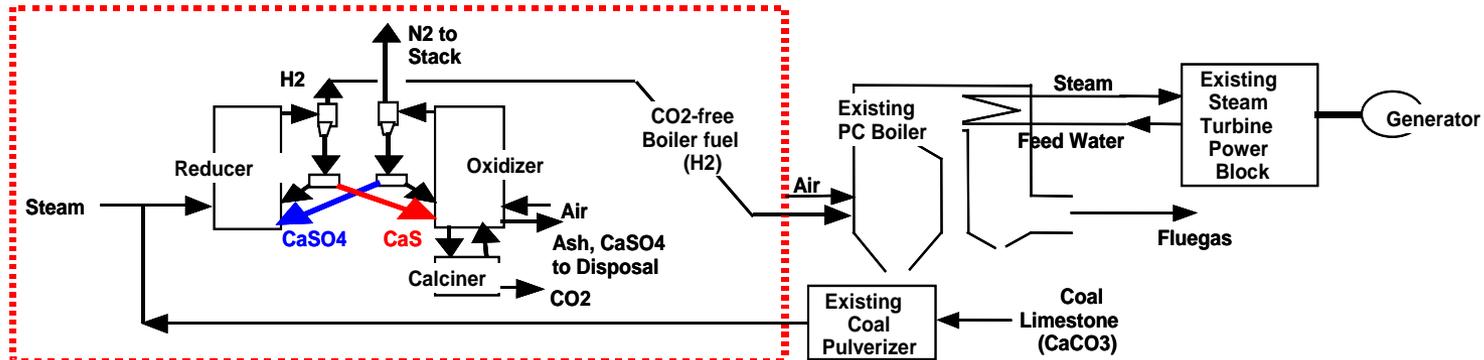
- CO<sub>2</sub> Capture – PC Retrofit
- CO<sub>2</sub> Capture – CFB Retrofit
- CO<sub>2</sub> Capture-Ready PC/CFB Power Plant
- Advanced Steam Cycles with CO<sub>2</sub> capture
- IGCC with CO<sub>2</sub> Capture
- Fuel Cell Cycles with CO<sub>2</sub> Capture
- Industrial Hydrogen with CO<sub>2</sub>

**Flexible technology with low cost**

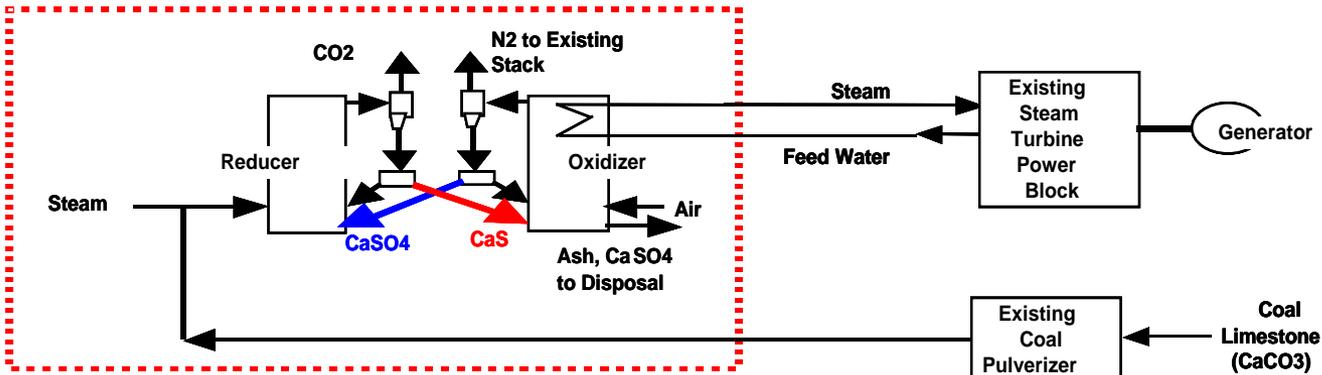
# Chemical Looping Overview

## Retrofit Options

### Pulverized Coal Power Plant - Retrofit Concepts



**Concept 1 – Chemical Looping CO2-free Fuel; Minimum Boiler Modification**



**Concept 2 – Chemical Looping Oxidizer Replaces/Modifies Boiler**

## Retrofit Options at < 20% Increase in COE with CO<sub>2</sub> Capture

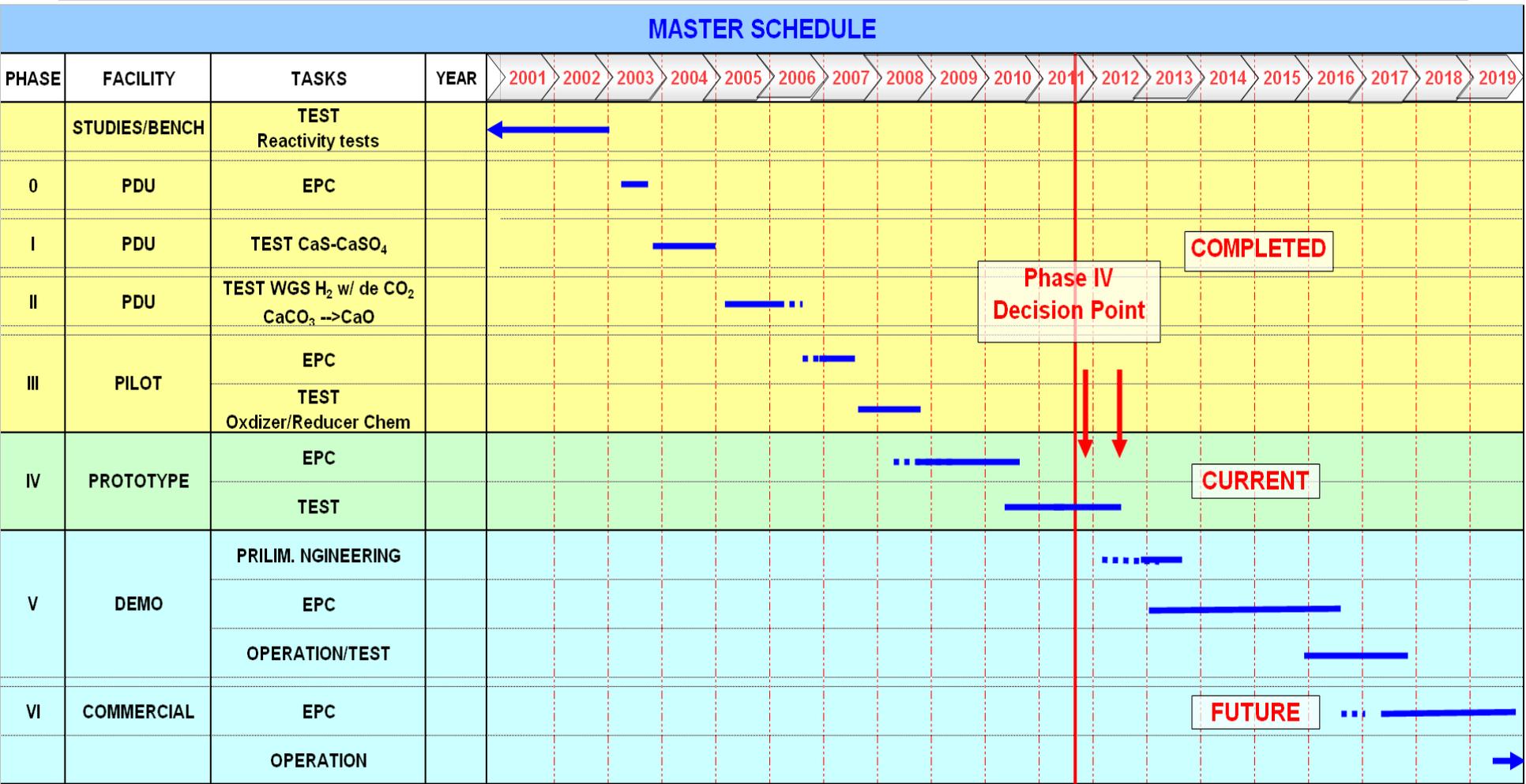
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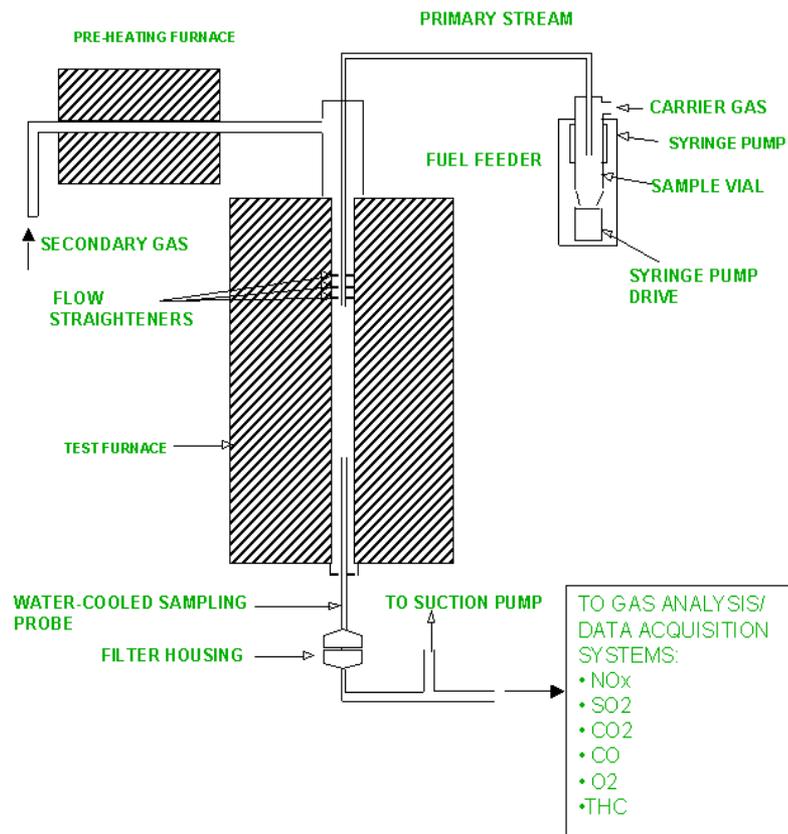
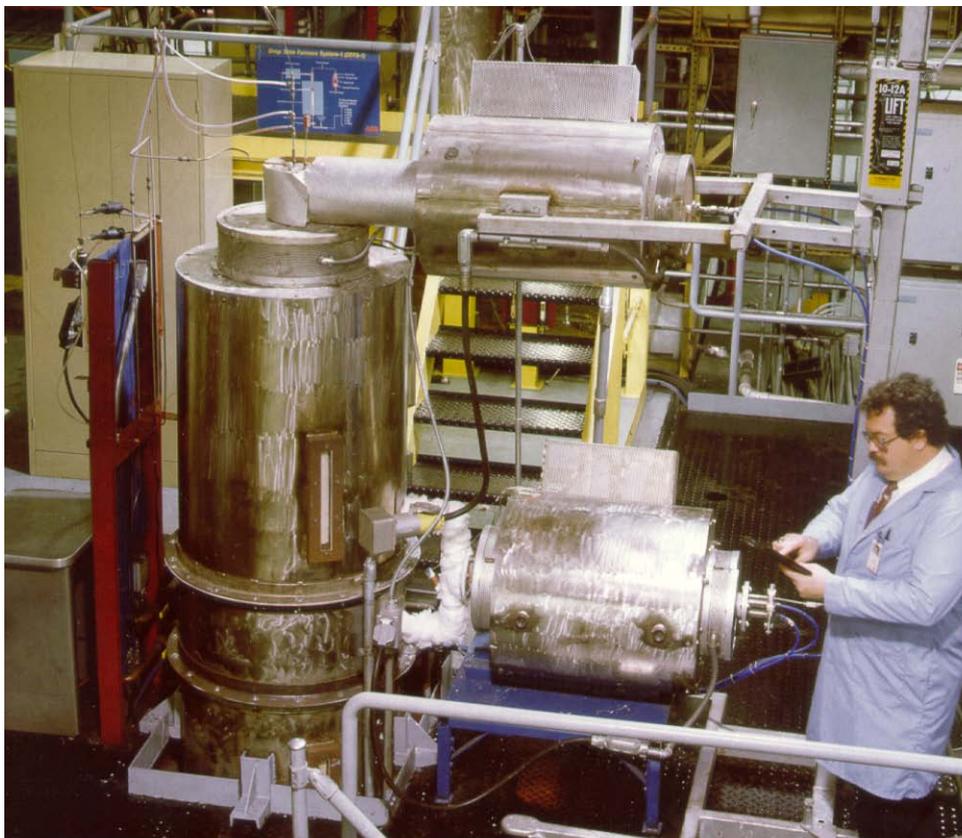
# Alstom – DOE Chemical Looping Development Plan



**Phases 0, I, II and III Completed Prior to October 2008. Phase IV Began October 2008 – First Coal Fire June 2011 –Autothermal Scheduled for September/October 2011**

# Chemical Looping Program

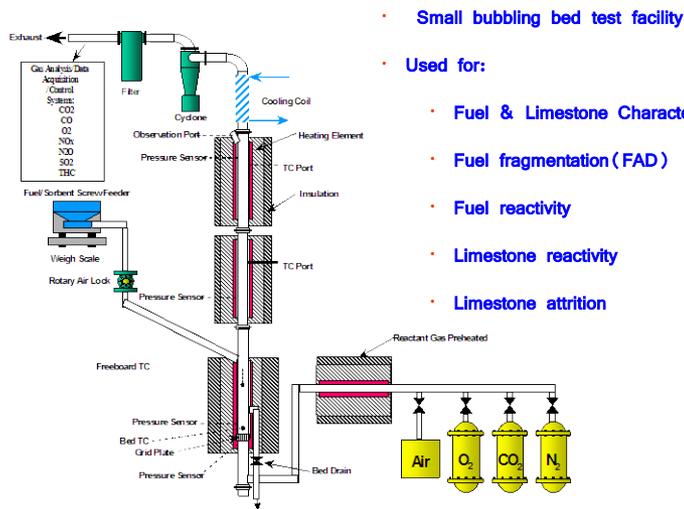
## Drop Tube Furnace System (DTFS) 1997 – 2003



**Schematic of Drop Tube Furnace System-1 (DTFS-1)**

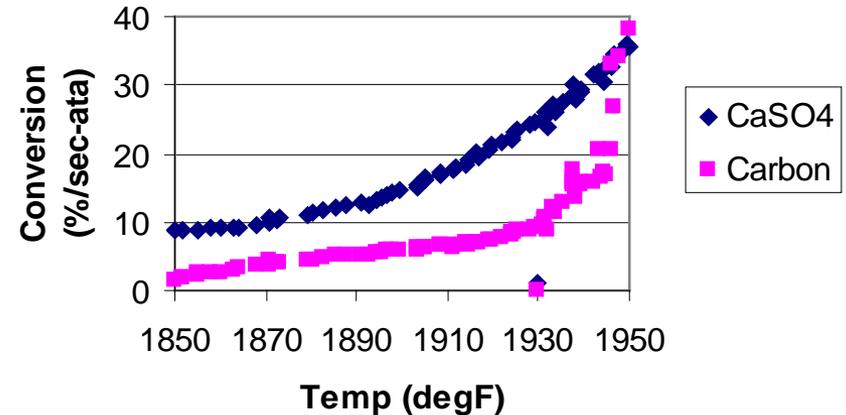
# Chemical Looping Program

## 4 Inch Fluidized Bed Reactor System (1999 – 2003)



- Small bubbling bed test facility
- Used for:
  - Fuel & Limestone Characterization
  - Fuel fragmentation (FAD)
  - Fuel reactivity
  - Limestone reactivity
  - Limestone attrition

### Reducer Kinetics 1000 micron

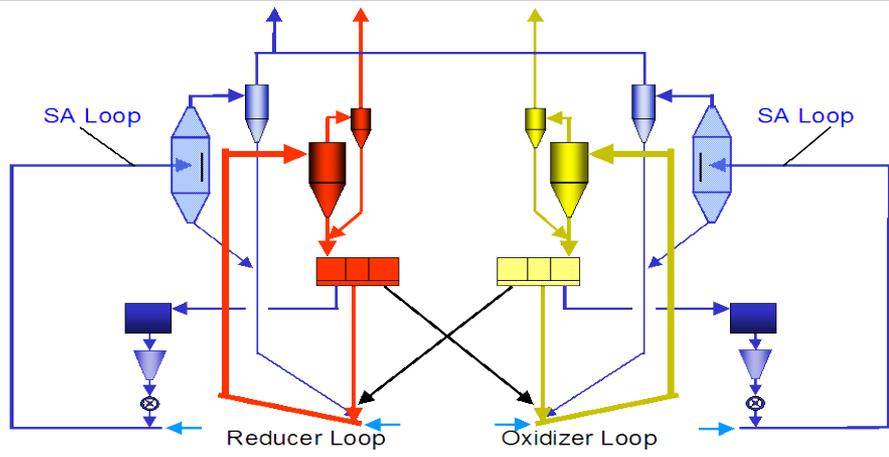


Work was completed in 2003 and was used together with DTFS data to determine Kinetic Rate Data

- Batch Tests Yield Reaction Rates Over a Wide Range of Temps and Compositions
- Basis for Equipment Sizing for Plant Cost and Economic Studies
- Basis for Chemical Looping Process Development Unit Design



# Chemical Looping Program Process Development Unit (PDU) 2004 -2008

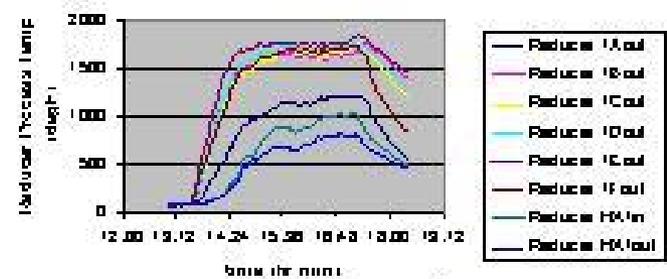


## Chemical Looping Process Development Unit (PDU)

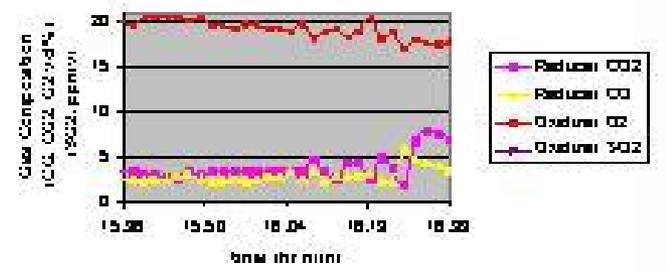
- Designed and Built by Alstom for about \$1M
- 2 Year Test Program - \$4M – 80% funded by US-DOE
- Allows Testing of Individual Loops and Processes



Ca-B-CaBO4 Cycling Test



Ca-B-CaBO4 Cycling Test



# Chemical Looping Program Summary of Kinetics Studies

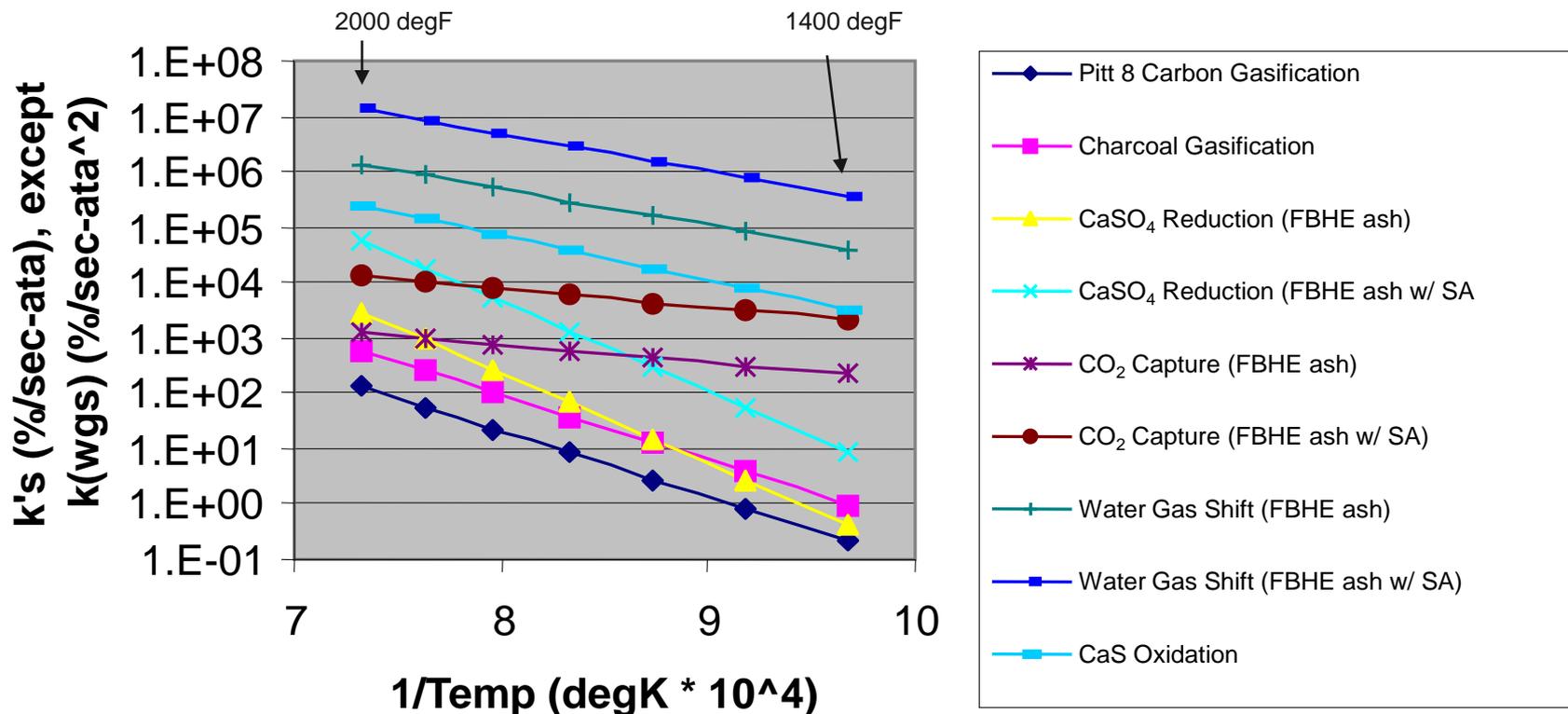


## Chemical Looping Reaction Kinetics Studies

Test Equipment	DTFS	4 Inch FBR	ChemLoop PDU	Fuels Tested
Particle size (micron)	50	1000	< 1200	
Reactions Studies				
1 Carbon Gasification (via CO <sub>2</sub> )	X (4)	X (2)		1. Pitt 8 Char 2. PRB Char 3. Wood Charcoal 4. 15 worldwide coals & chars 5. Gypsum 6. CFB Ash 7. Reduced CFB ash 8. Chemstone Limestone 9. Marblewhite Limestone
2 Carbon Gasification (via CaSO <sub>4</sub> )		X (2)	X (1,3)	
3 Devolatilization	X (4)	X (1,2)		
4 CaS Oxidation	X (4)			
5 CaSO <sub>4</sub> Reduction		X (5)	X (6)	
6 CaO CO <sub>2</sub> Capture	X (9)	X (8)	X (8)	
7 WGS		X	X	
8 WGS (w/ CaO)		X (6)	X (6)	
9 CaS Oxidation	X (6,7)	X (5)	X (7)	

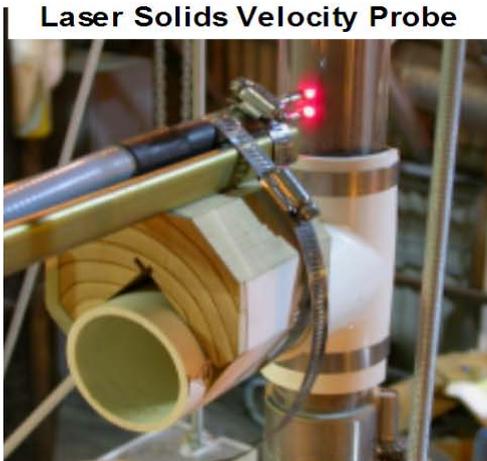
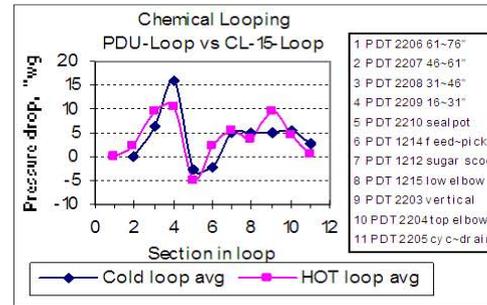
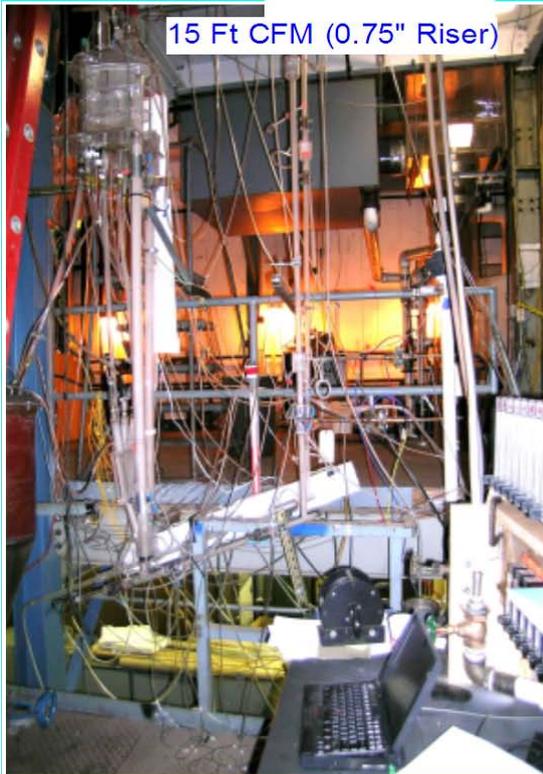
Extensive Kinetic Studies Performed To Size The Prototype

### Chemical Looping - Kinetics Summary



Extensive Kinetic Studies Performed To Size The Prototype

# Chemical Looping Cold Flow Model (CFM)



- Goals for the CFM:
  - Distribute, Transport, and Control Solids Flow
  - Scale-up
  - Training, Operating, and Trouble Shooting

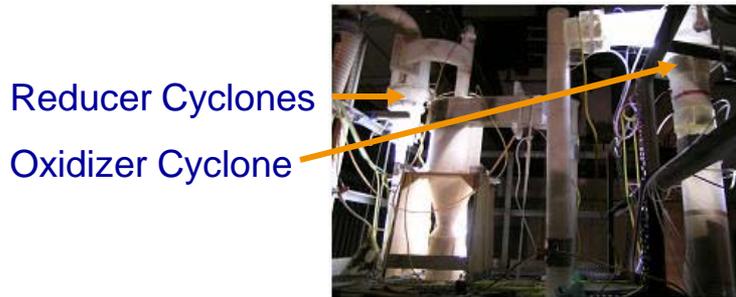
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# ALSTOM's Chemical Looping 40ft Cold Flow Model (CFM)



Reducer Cyclones  
Oxidizer Cyclone



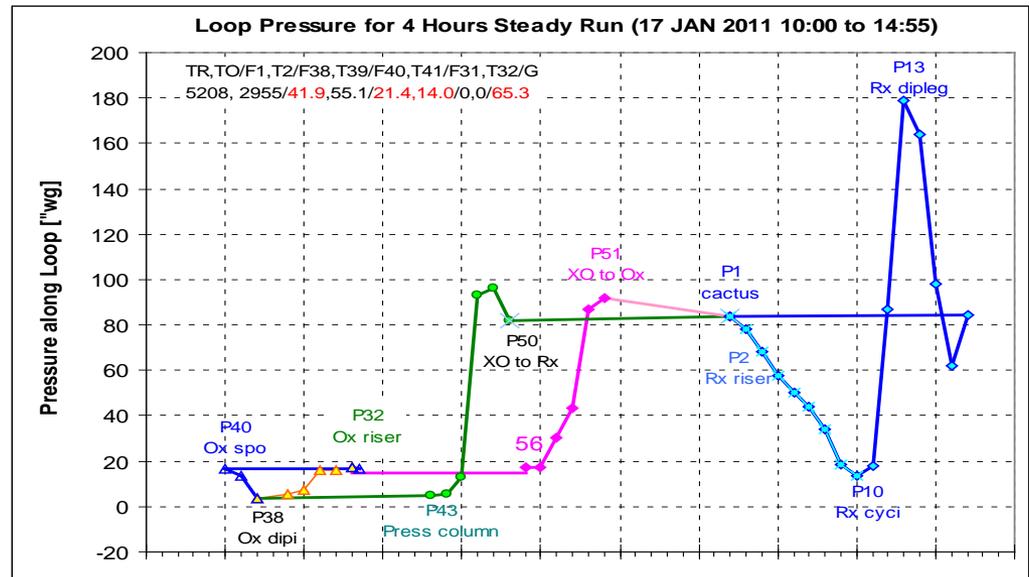
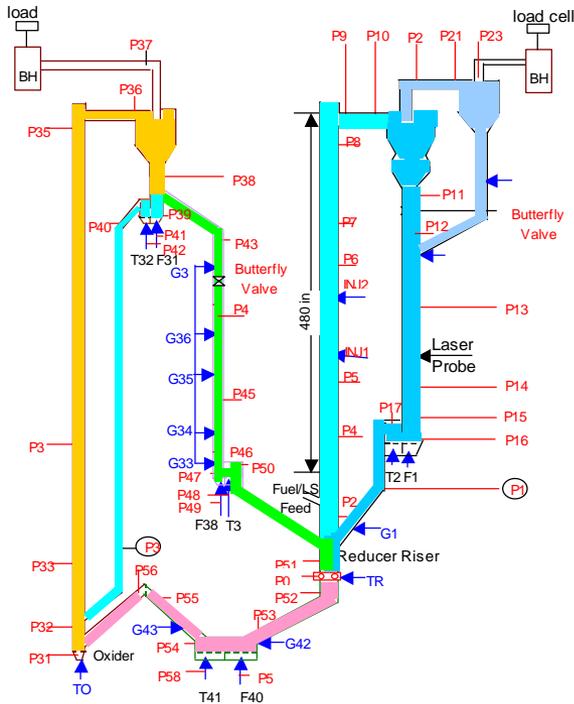
Oxidizer Riser  
Pressurizing Column from Oxidizer to Reducer  
Reducer Riser  
Reducer Dipleg



Reducer SPCV  
Pressurizing Column SPCV  
Cactus  
Reducer Inlet Air  
Crossover from Reducer to Oxidizer

# ALSTOM's Chemical Looping - CFM

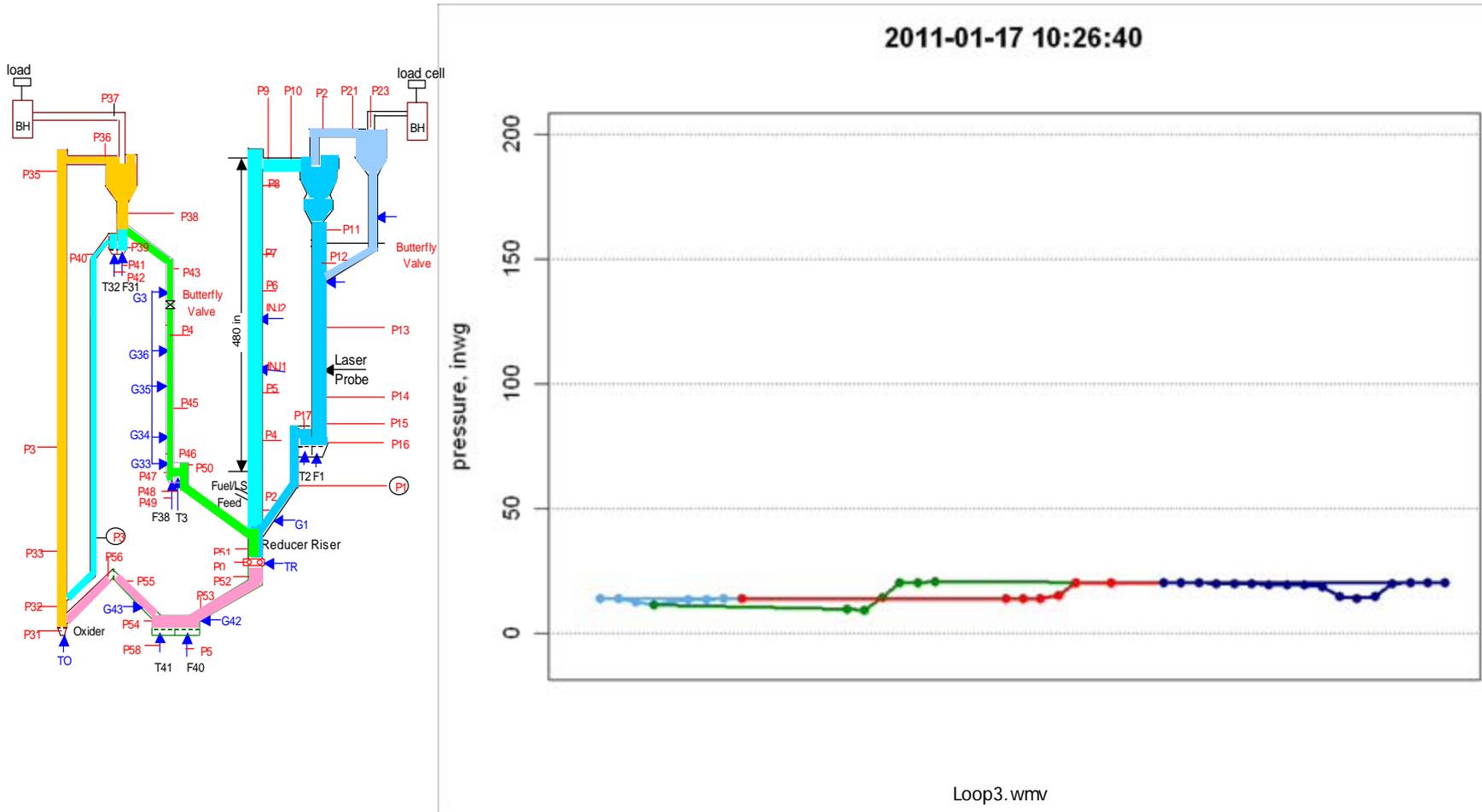
## 4 Hours Steady Operation – Pressure Balance



4 Hours of steady Operation

# ALSTOM's Chemical Looping - CFM

## 4 Hours Steady Operation



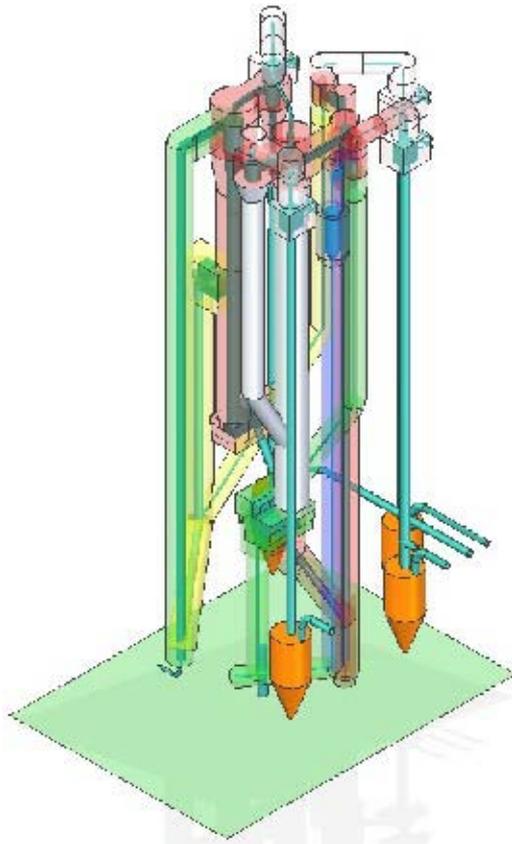
Solids flow and pressures around the loop remain steady during operation.

# Chemical Looping - CFM Summary

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- CFM validated the Prototype's solids transport concept
- Multi-loop CFM operation was demonstrated:
  - start-up and shutdown
  - control stability of the system
- Data used to verify the scale-up method
- CFM used for the training of operators for the prototype unit
- CFM will be used to trouble shoot Prototype solids transport

## Chemical Looping 3 MWt Prototype Concept



- Up to 1000 lb/hr coal flow
- 1<sup>st</sup> Integrated Operation
- 1<sup>st</sup> Autothermal Operation

### Prototype:

- Location – Alstom Power, Windsor, CT.
- All Equipment Necessary for Viable Demo Design
- Design, Construction, Operation, Maintenance, Modification by Alstom



# Chemical Looping Prototype Component Construction



Secondary Cyclone

Primary Cyclone

Diplegs

Main Seal Pot

Fluidizing Section

Reducer to Oxidizer  
Crossover

MTF – New Refractory Lining

Upper Seal Pot

Reducer Spool Pieces

Lower Seal Pot

Reducer Cactus



The Prototype was  
integrated into the  
existing Multi-use  
Test Facility (MTF)



# Chemical Looping Prototype Components Installed



## Product Gas Condenser/Chiller

Removes water from the product gas  
and protects Recycle Gas Compressors



Recycle Gas Compressor supplies  
fluidizing gas for the SPCV's

# Prototype Startup



**Main Control Room Operating station**



**Control System Programming Station**

**Prototype startup in progress**

## The Prototype project has made significant progress toward achieving fully integrated operation.

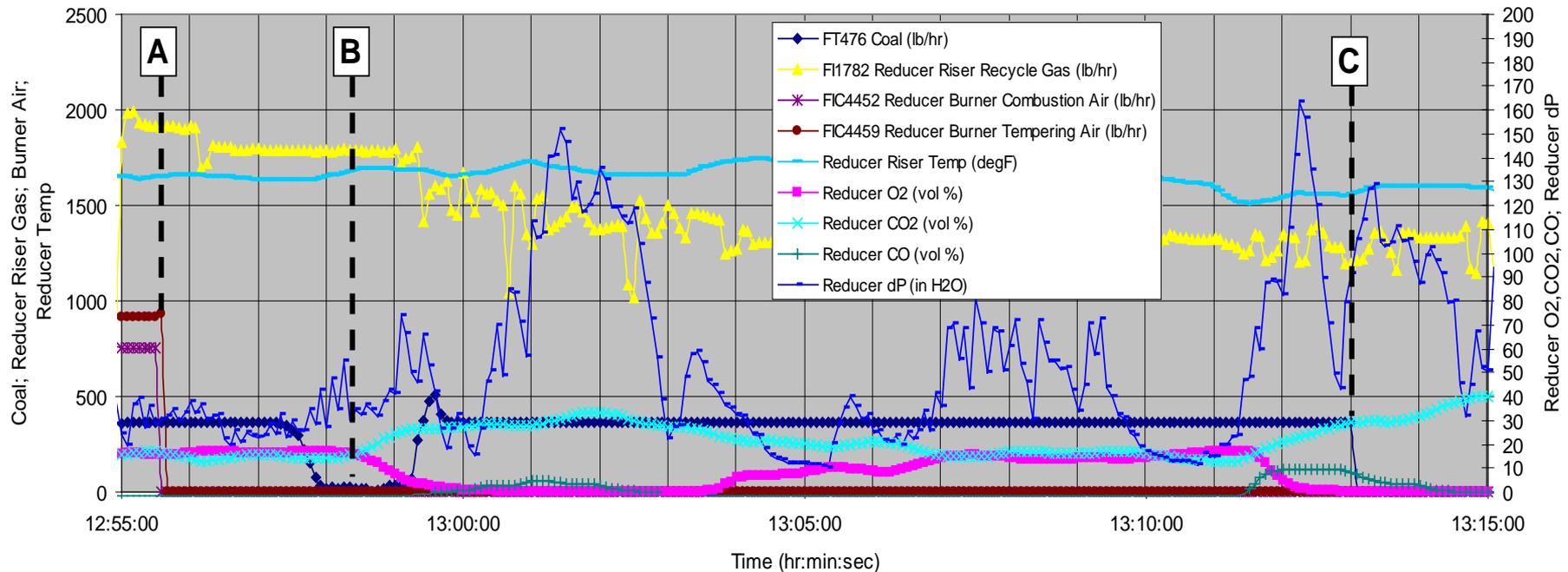
- Controlled solids recirculation in the cold flow model and the prototype.
- Online heat-up of the process by external electric heaters, external natural gas burners and direct injection of natural gas into the reactors.
- Coal firing at relatively low reactor temperatures with low tar formation.
- Coal firing at design temperature with no evidence of tar formation.
- Coal and sorbent feeding online.
- SAHE operation.
- Hot restart after main fuel trip.
- Production of CO<sub>2</sub> (Option 1) and Syngas (Option 2).
- Combustion reactions with chemical looping reactions.

**Chemical looping reactions were achieved on June 11, 2011**

# CaOx - Chemical Looping Prototype Results



Reducer Performance

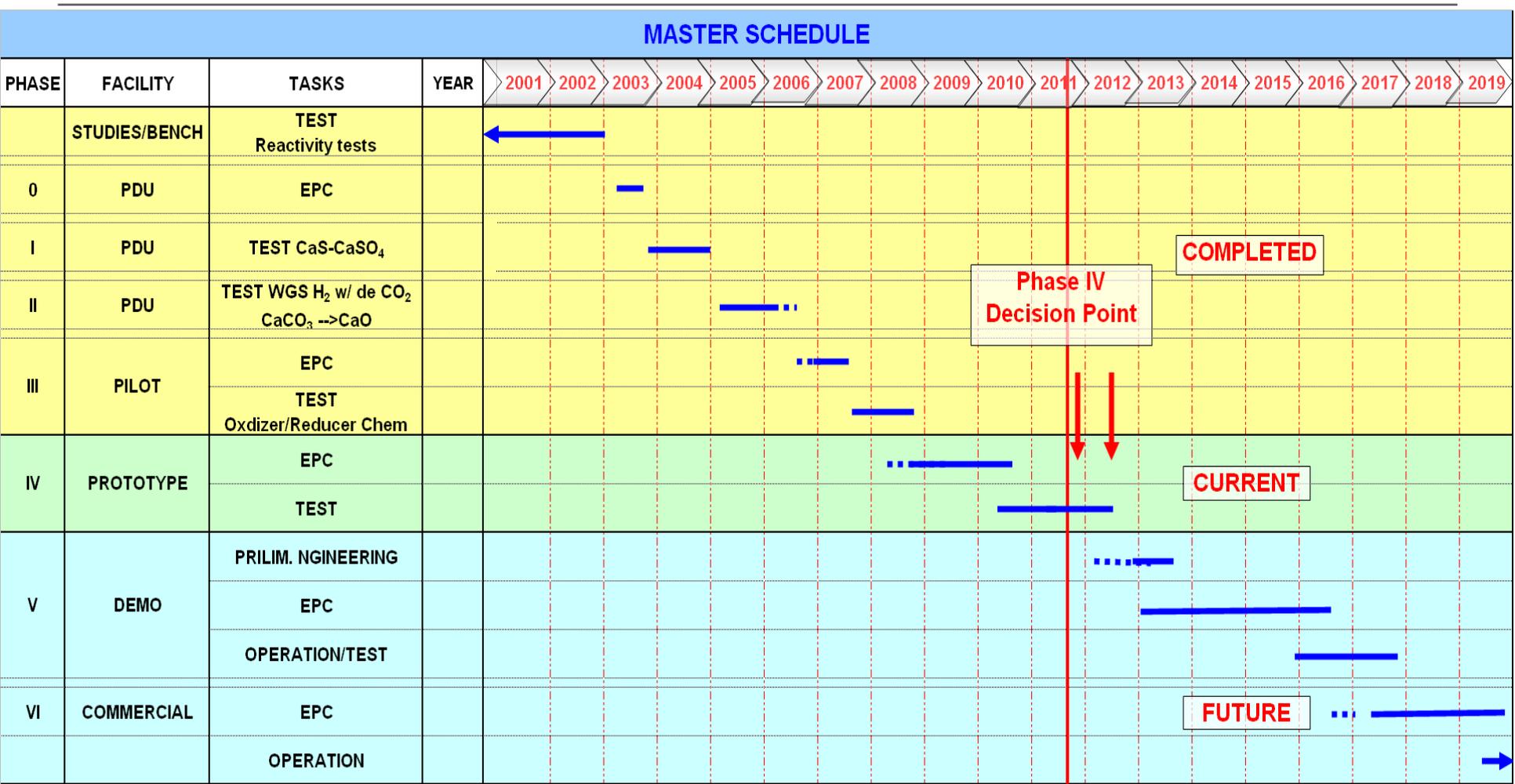


- Point "A" - 360 lb/hr of coal and 1900 lb/hr of air for solids transport were flowing to the reducer
- Point "A" to Point "B" - CO<sub>2</sub> concentration is about 35% vol.
- Point "C" - The recycle intake was switched from air to recycled product gas. The CO<sub>2</sub> slowly rises as N<sub>2</sub> is washed out of the system

Chemical looping reactions were achieved on June 11, 2011

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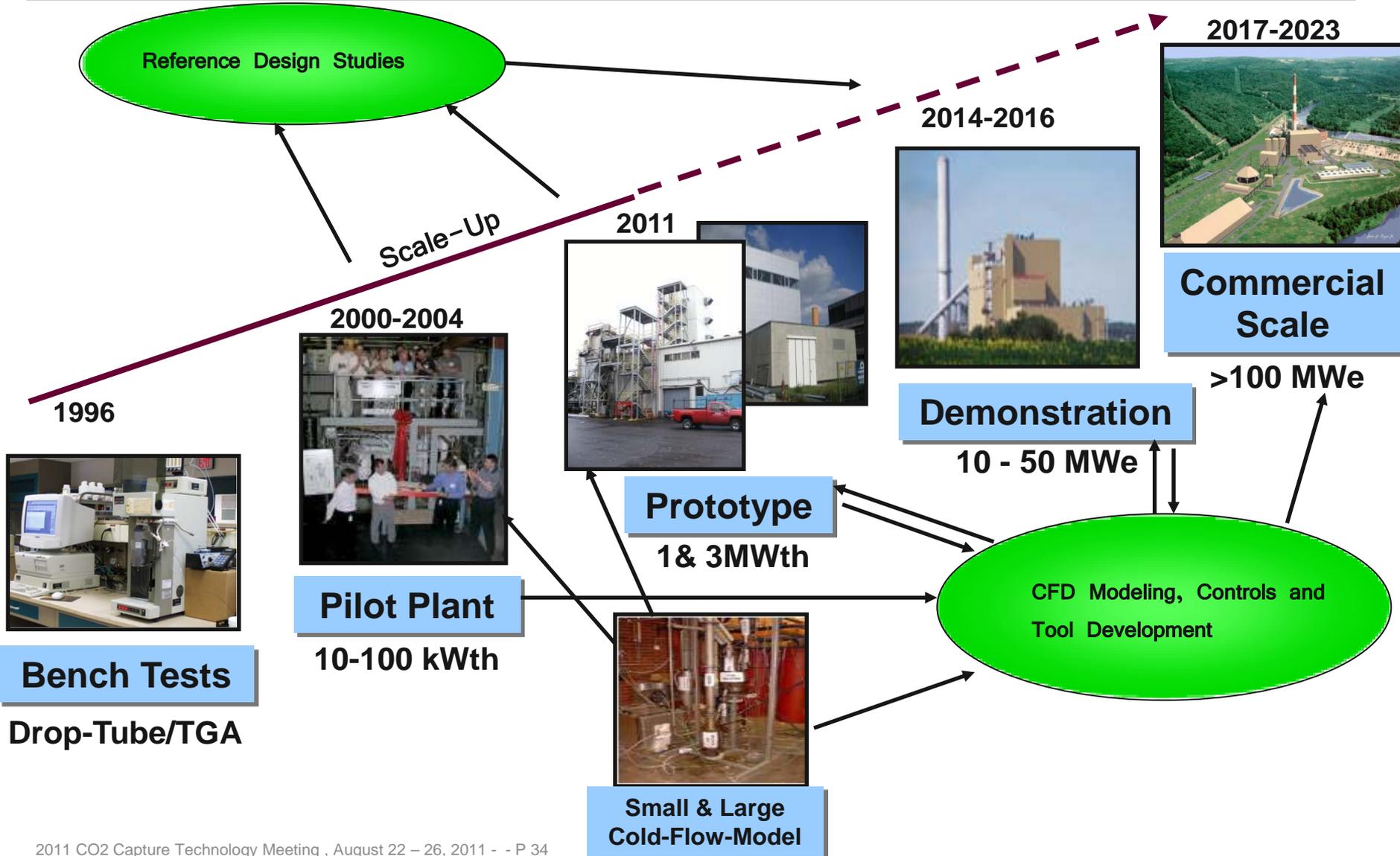
# Alstom – DOE Chemical Looping Development Plan



## Next Steps – Demonstration and Commercial Projects

- Phase IV A
  - Auto-Thermal 40 hour Coal Operation
  - Optimization Test
- Phase IV B
  - Options: Syngas, H<sub>2</sub>
  - Add and test Calciner
- Phase V
  - Demonstration Plant
- Phase VI
  - Commercial Plant

# Alstom - Chemical Looping Process Development Steps



Any Questions?

[www.alstom.com](http://www.alstom.com)

**Thanks to DOE-NETL!**



**ALSTOM**